



Specialist for Pumping Technology

Session 39 – Introduction to Positive Displacement (Plunger) Pumps

Simon Smith February 2025





Presenter Profile – Simon Smith

Simon graduated with an honours degree in Chemical Engineering from the University of Surrey in 1978 and began a long career in the engineered pump industry spanning 44 years (so far!) with Peerless Pump, BW/IP International / Flowserve, SPP Pumps, Ruhrpumpen and Ebara Cryodynamics.

Over his long career he has filled various roles as Applications Engineer / Manager, Project Manager, Key Account Specialist, Vertical Pump Product Specialist, International Sales Engineer / Manager / Director and he has considerable experience in Training & Mentoring young engineers.





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- No 27 – The Importance of System Curves
- No 28 – NPSH & Nss Made Simple
- No 29 – Curve Shape, Head Rise & Allowable Tolerances
- No 30 – Selecting the Right Pump for the Application
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- No 32 Pump Instrumentation
- No 33 Handling Viscous Fluids with Centrifugal Pumps
- No 34 Fire Pumps for the Oil & Gas Industries
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- No 36 Engineered Systems
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**QUALITY
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- Q&A Report

Session 39 – “Introduction to Positive Displacement (Plunger) Pumps”

Aimed at Process and Mechanical Engineers, and Consultant Engineers who specify pumping equipment as well as Applications & Sales Engineers selecting and quoting them.

Pump engineers are generally knowledgeable about centrifugal pumps, but are less familiar with positive displacement pumps. This session will look at PD pumps in general but with particular focus on reciprocating plunger pumps.

SECTION 1

- 1- POSITIVE DISPLACEMENT VS CENTRIFUGAL
- 2- WHAT IS A RECIPROCATING PUMP?

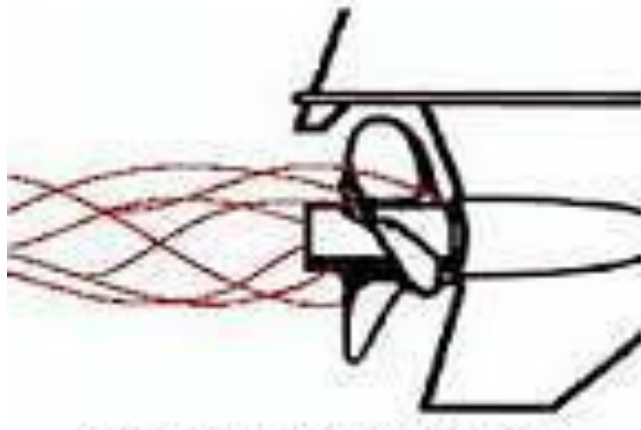
SECTION 2

- 3- RUHRPUMPEN RDP PUMP
- 4- TESTING
- 5- PACKAGE OPTIONS



Section 1 Part 1- POSITIVE DISPLACEMENT VS CENTRIFUGAL

How is flow generated? (Different thermodynamic process)

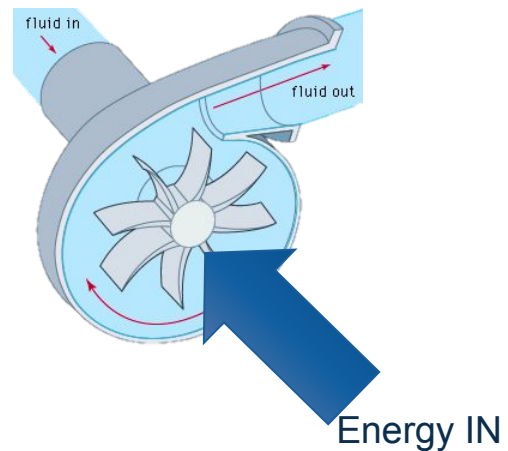


Inputs energy directly to
liquid ($\dot{W}_{in}$)

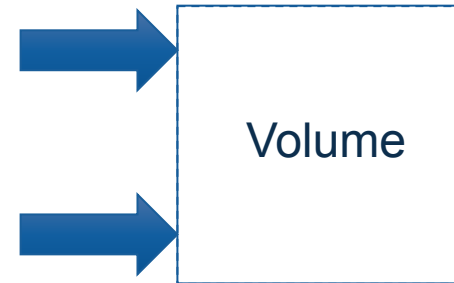


Moves the boundary of
the liquid

How is the flow generated? (Different thermodynamic process)



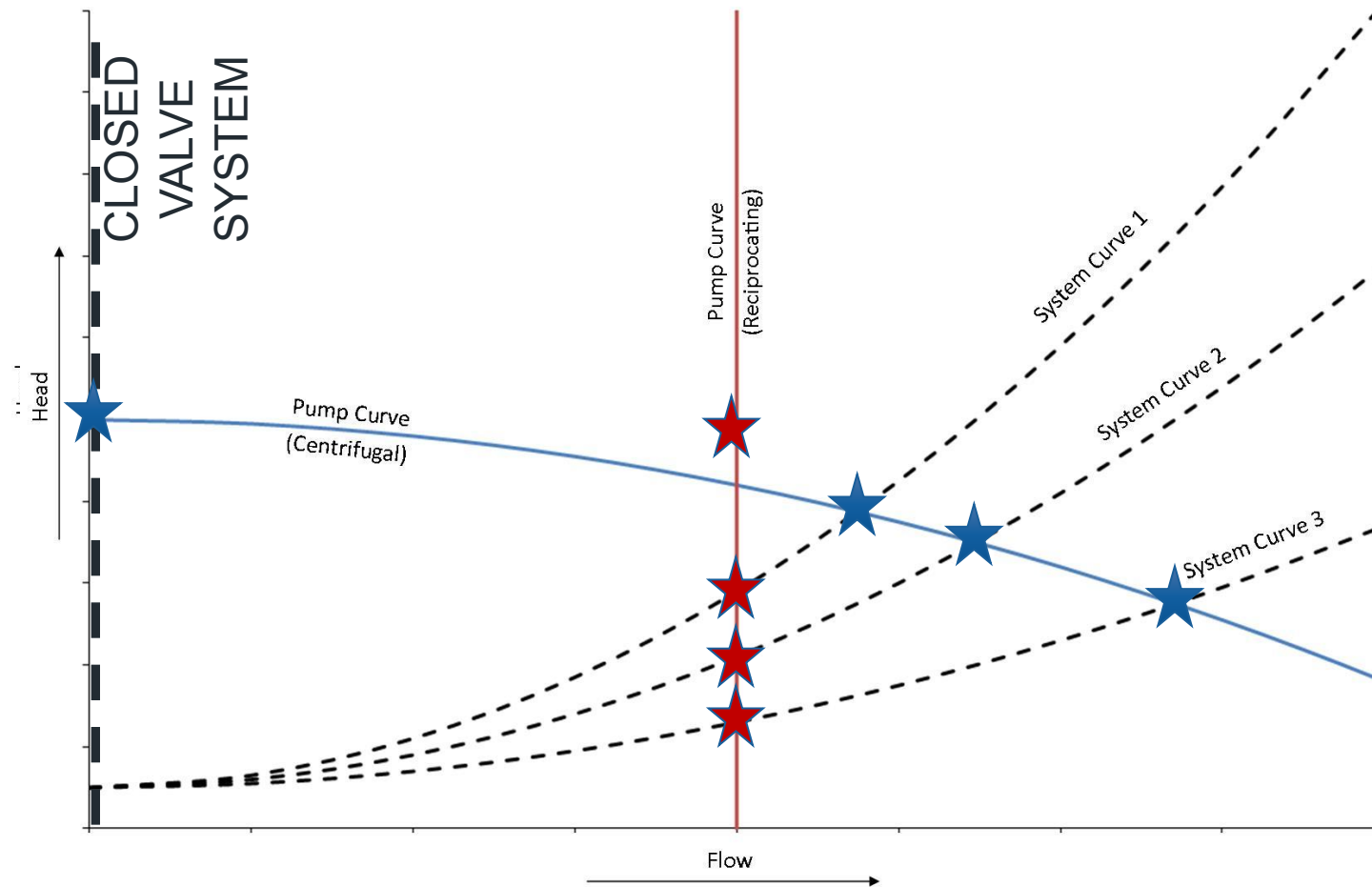
Inputs energy directly to
liquid ($\dot{W}_{in}$)



Moves the boundary of
the liquid.

Flow = swept volume of
cylinder x number of
plungers

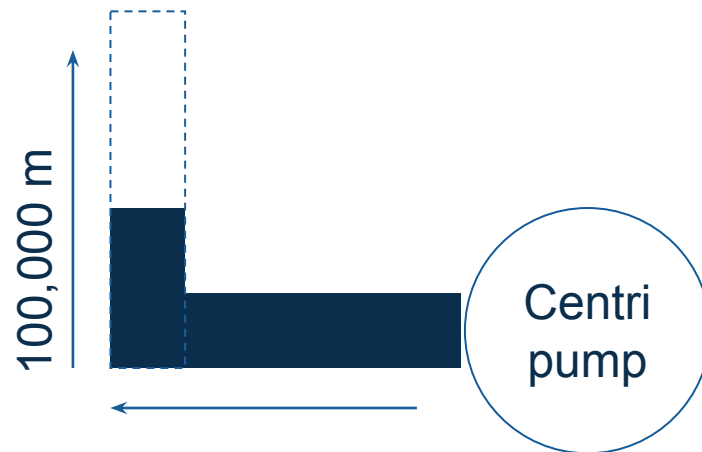
- Flow is constant for a fixed speed pump



Centrifugal Pump

Discharge head determined by pump hydraulics

Maximum head is limited

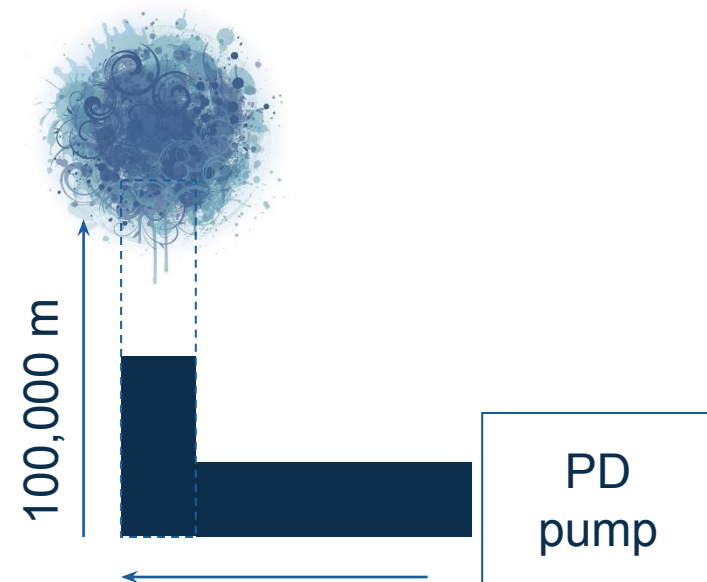


Reciprocating Pump

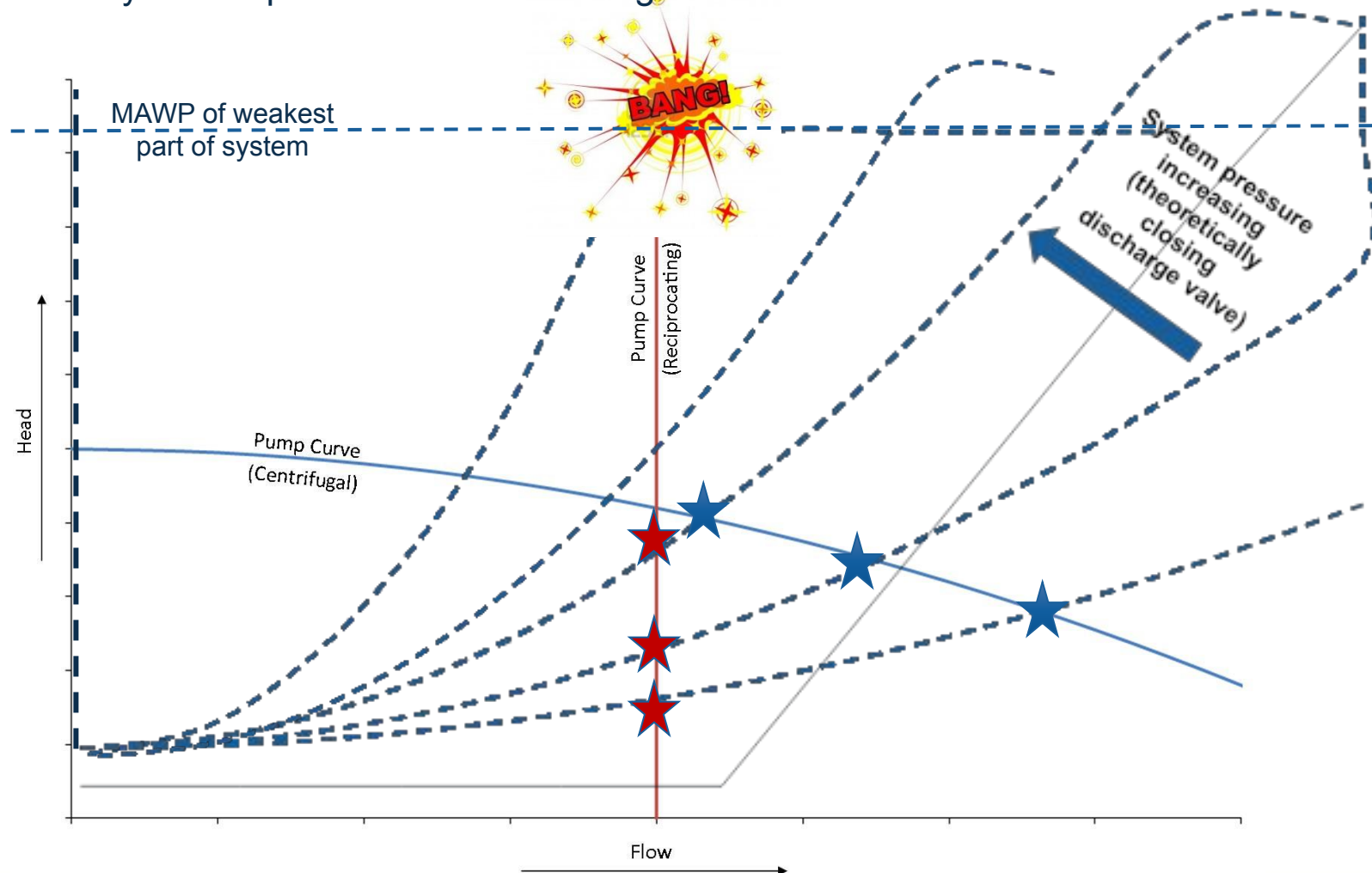
Discharge head determined by system back pressure

Head increase unlimited – theoretically infinite head at closed valve

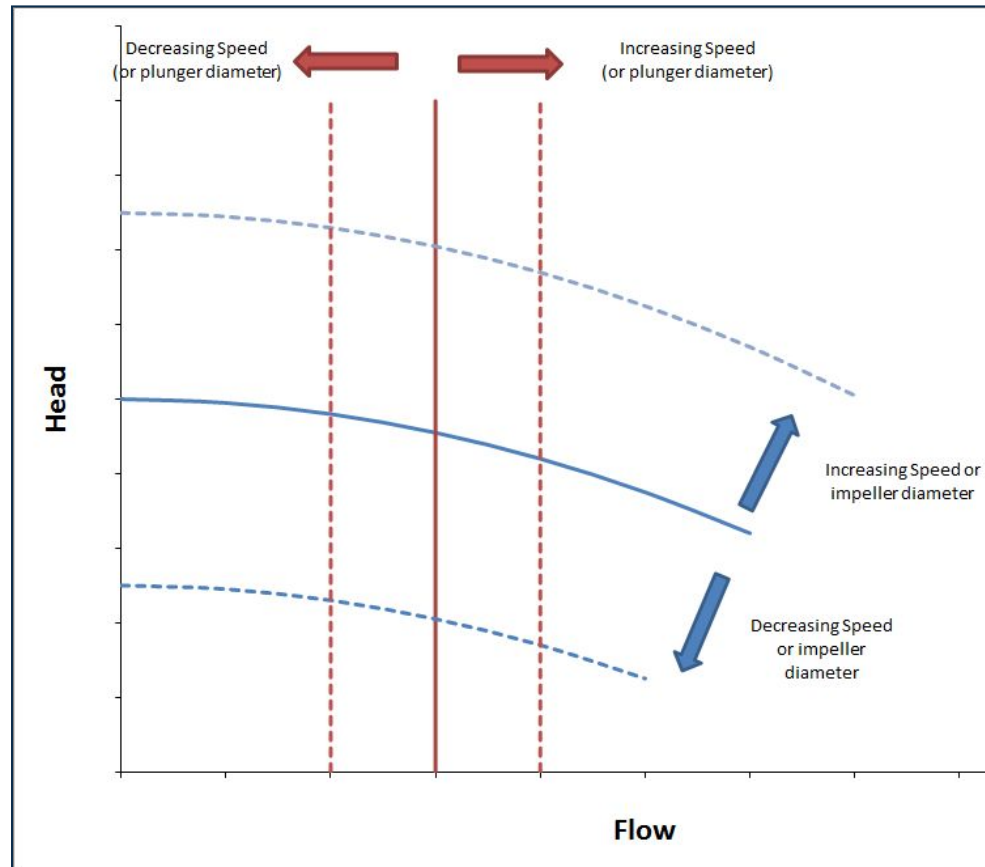
Until failure of weakest part of the system



- Theoretically infinite pressure when discharge valve is closed



SPEED EFFECT



PD pump flow is fixed for fixed speed

Flow varies directly with speed

Maximum Speed as defined by API 674

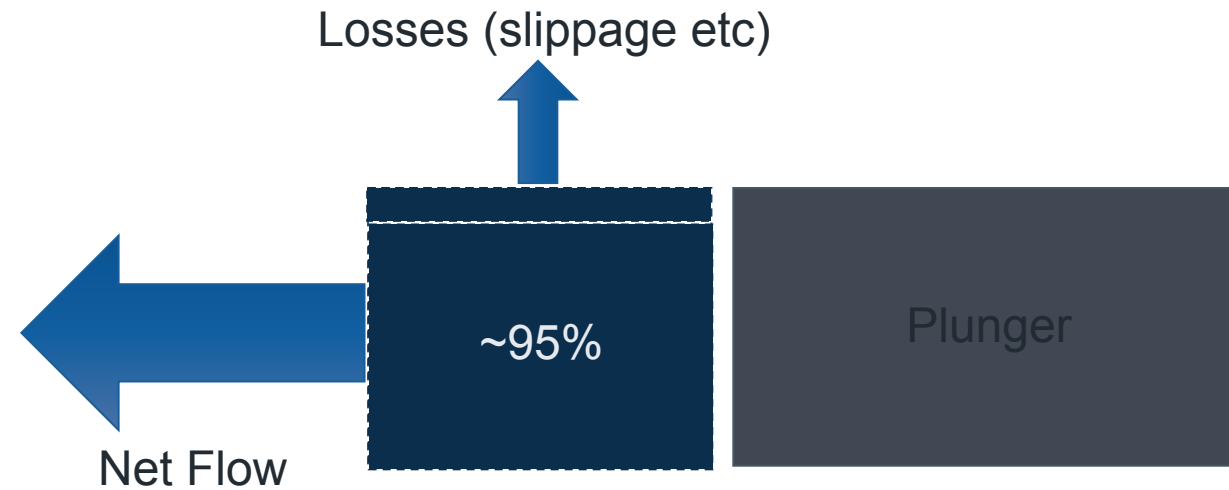
Stroke mm	50	70	100	150	200
RPM	450	400	350	270	210

(RPD design allows us to run faster for non-API applications = smaller pump)

Efficiency for PD pump is fixed and does not change for changing flow/head.

RDP efficiency is approximately 98%.

API 674 states that we cannot use more than 95% for power calculation



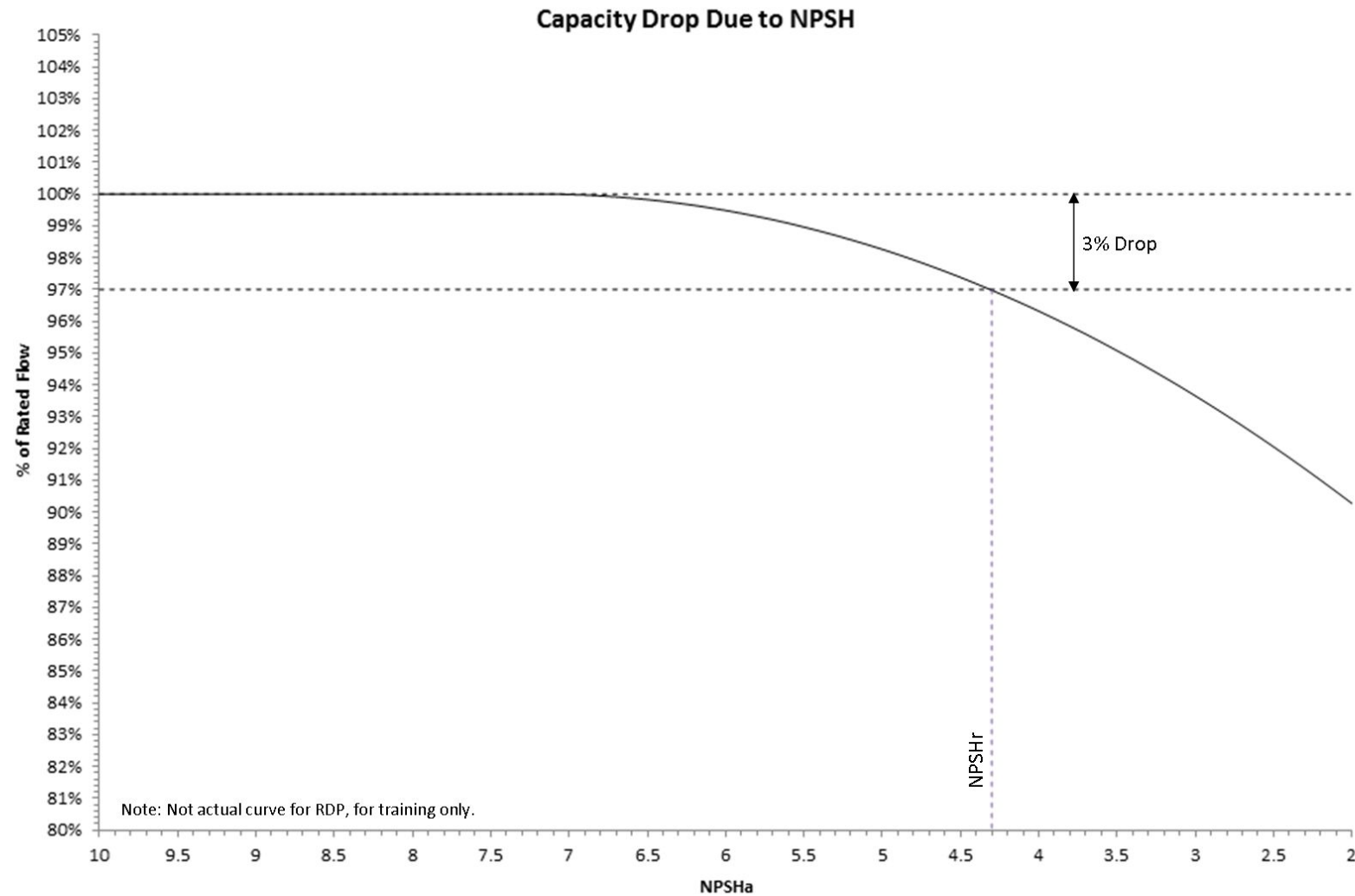
Estimate $\text{Power (kW)} = \text{Pressure (bar)} \times \text{Flow (l/m)} / 540$

Per API674 - Motor is sized in order to be at least 110% of the greatest power required for any of the specified operating conditions (including gear & coupling losses).

So normally it is 110% of the pump absorbed power at rated flow and at the relief valve set pressure.

- NPSHA = **NET POSITIVE SUCTION HEAD AVAILABLE**
- NPIP = **NET POSITIVE INLET PRESSURE**
- NPIP and NPSHA are the same thing. NPIP is in terms of pressure and NPSHA is in terms of head. Either can be seen on API674 datasheet.
- Same principle as NPSHA and NPSHR in a centrifugal pump
 - High enough pressure when liquid is accelerated to avoid cavitation
- Also specifically for reciprocating pump ...
 - NPSHA has to provide force needed to open valves and adequately fill the cylinders
 - Criteria is 3% FLOW drop (compared to 3% HEAD drop in centrifugal pump)
 - Note API 674 states that NPSHa should have a minimum of 1m margin to NPSHr
- Results of low NPSH margin
 - Erratic and unreliable performance
 - Reduced flow (in extreme cases!)
 - Erosion of plungers and valves due to cavitation
 - Noise

NPSHr (required)



Centrifugal pump power IS affected by SG (lifting something heavier uses more muscle!!)

$$\text{Power} = \frac{\text{Head} \times \text{Flow} \times \text{SG}}{\text{Efficiency} \times C}$$

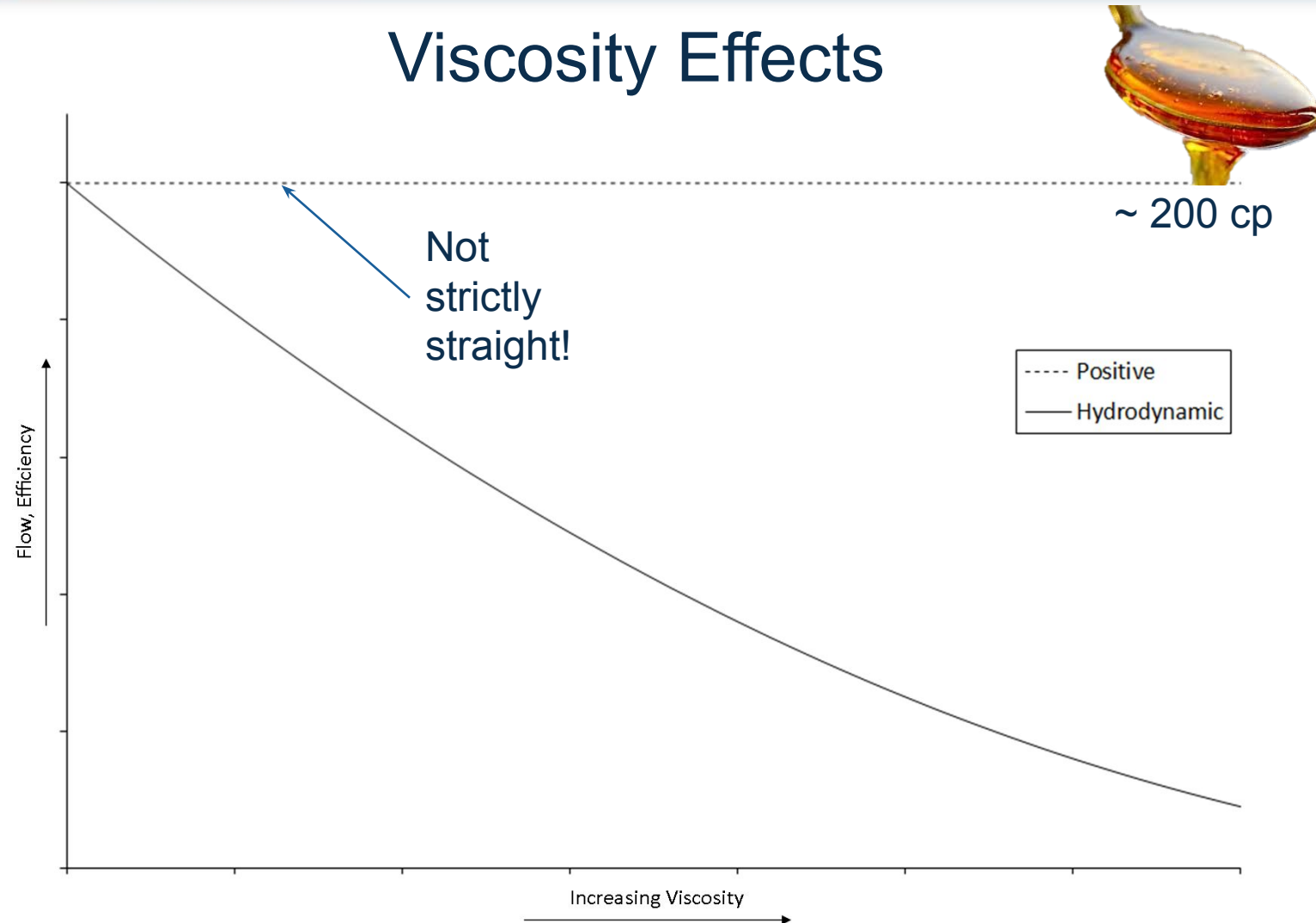


Reciprocating is NOT affected (pushing 1m³ of feathers and 1m³ of lead from 1 point to another on a frictionless surface uses same energy!)

Estimate

$$\text{Power (kW)} = \frac{\text{Pressure (bar)} \times \text{Flow (l/min)}}{540}$$

Viscosity Effects





Things to remember

- ✓ Flow rate => Determined by pump
- ✓ Suction/discharge pressure => Determined by system
- ✓ Discharge pressure is only limited by the power supplied to the pump and structural limits of the weakest component.
 - Fluid head
 - Power end
 - System
- ✓ A plunger pump does not create pressure
- ✓ The system generates the pressure
- ✓ The pump, pumps against this pressure





Section 1 Part 2- WHAT IS A RECIPROCATING PUMP?

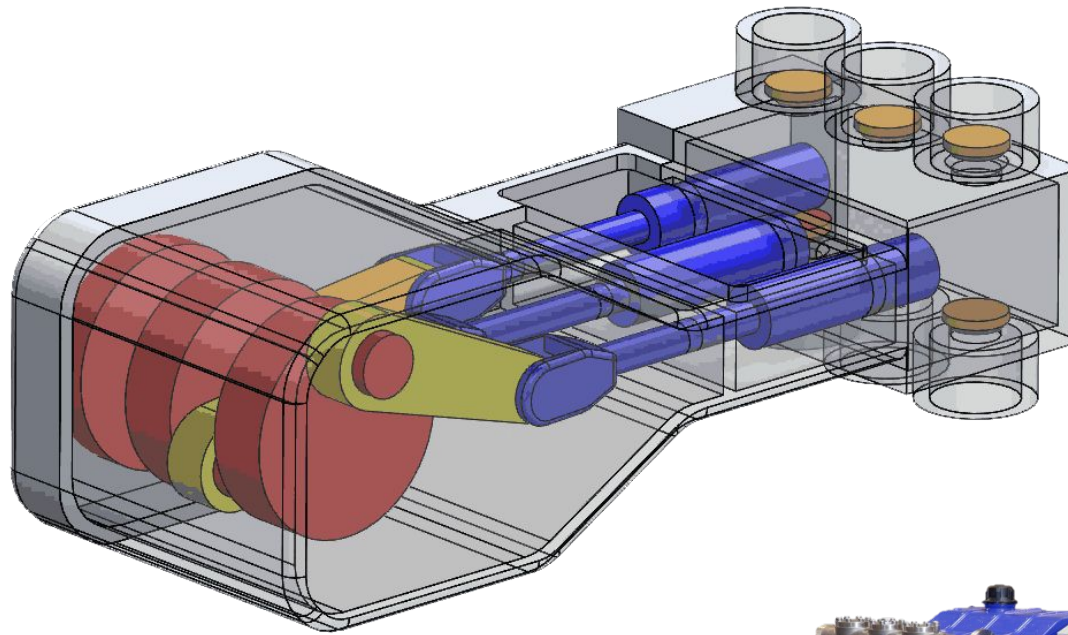
What is a Reciprocating Pump?

A pump that moves a known quantity of liquid with each stroke of a plunger



RDP OVERVIEW

THE RDP IS....



✓ **Plunger Pump**

✓ **Power Pump**

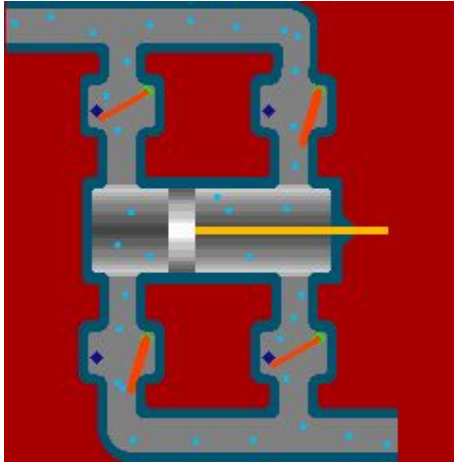
✓ **Single Acting**

✓ **Horizontal layout**

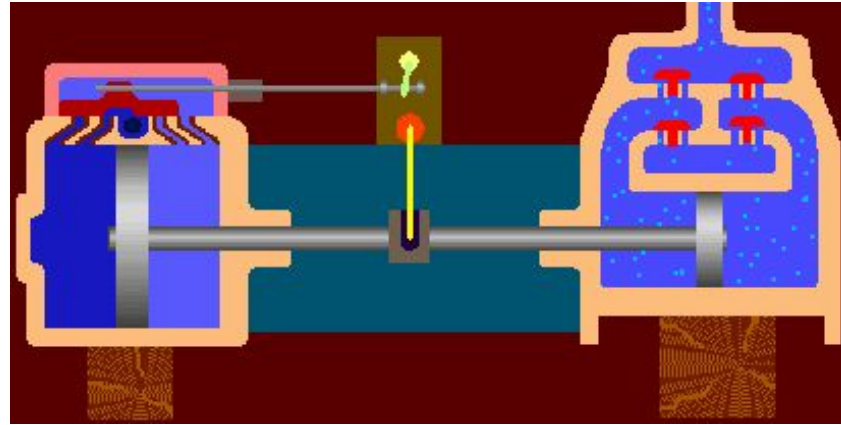


RDP OVERVIEW

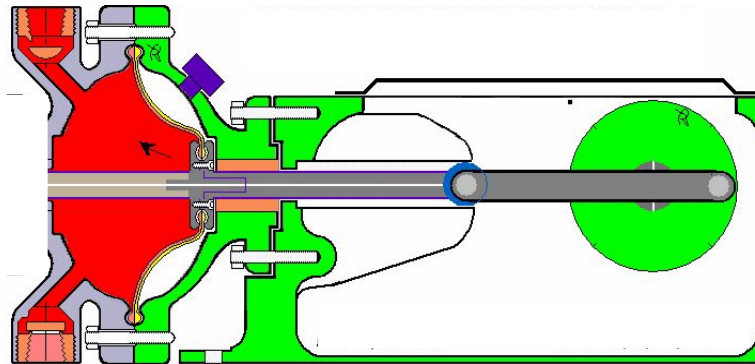
RDP IS NOT ...



Double Acting



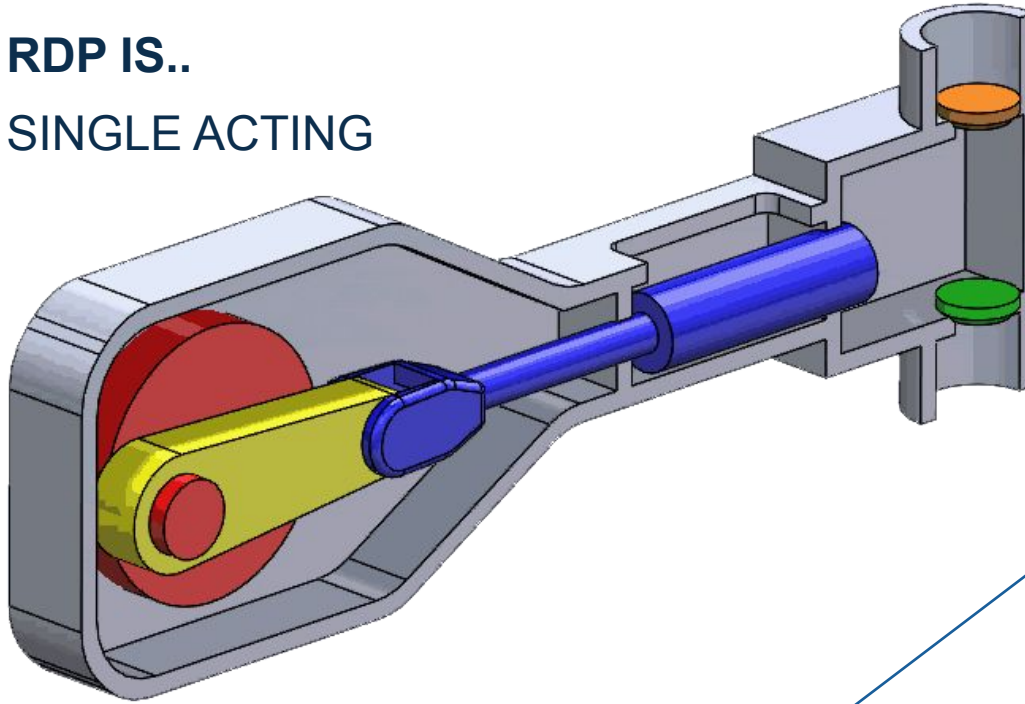
Direct Acting



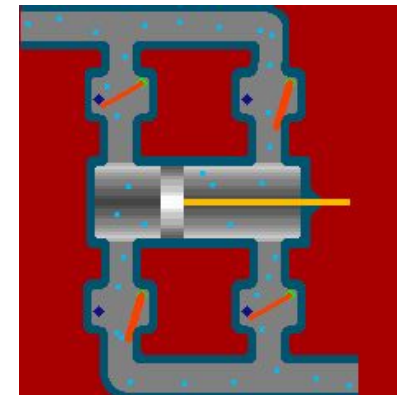
Diaphragm Pump

RDP OVERVIEW

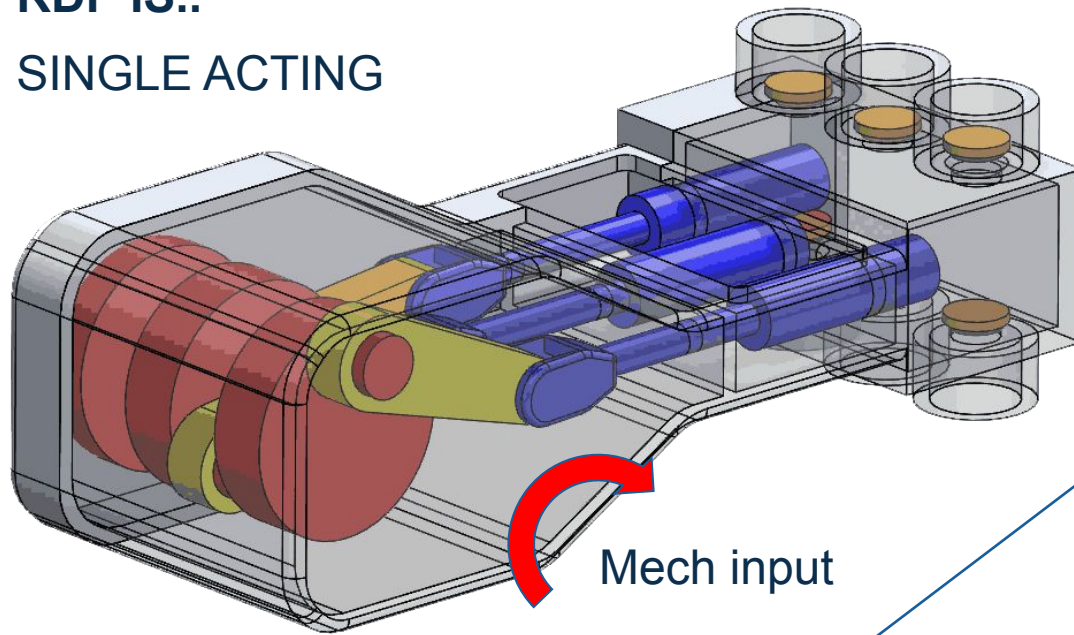
**RDP IS..
SINGLE ACTING**



**RDP is not..
Double acting**



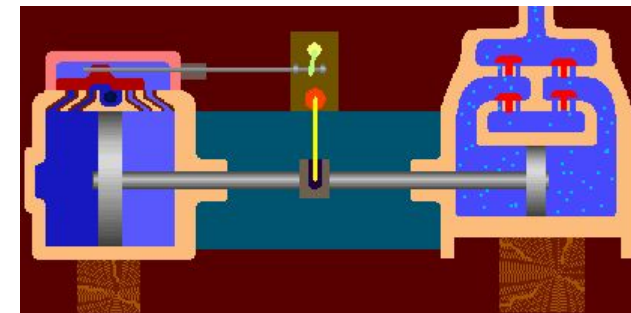
**RDP IS..
SINGLE ACTING**



**RDP is not..
Direct acting**

Media

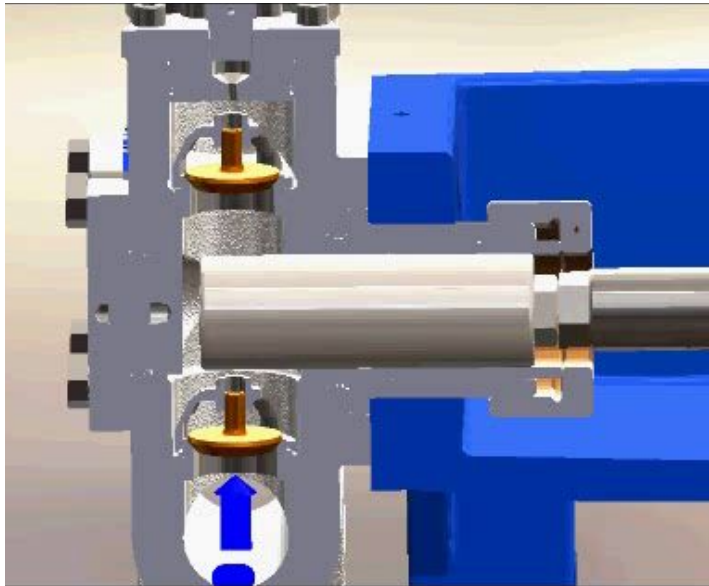
Steam



PLUNGER PUMP (RDP)

Sealing elements **FIXED** in a stuffing box, plunger moves through packings

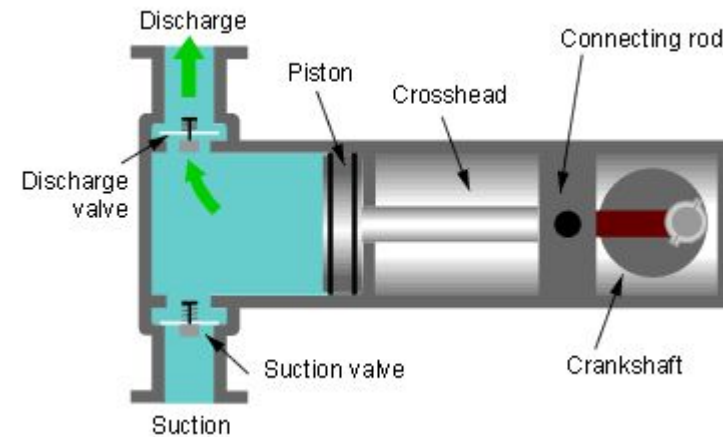
- Higher pressure/lower volume



PISTON PUMP

Sealing elements **MOVE** with a piston

- Higher volume/lower pressure



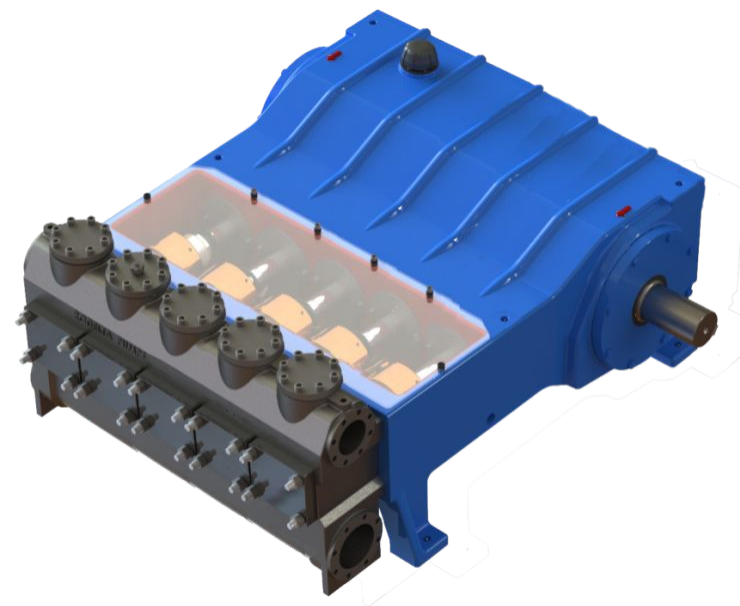
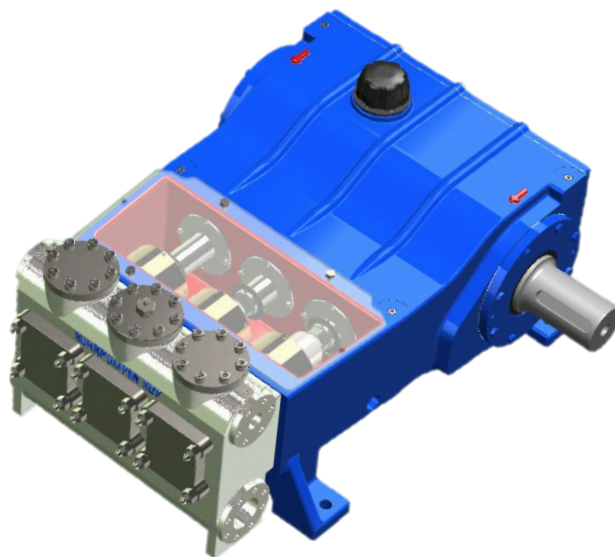
<http://engineering.stackexchange.com/>

Both types of pumps are covered by API 674

Reciprocating Pump Characteristics

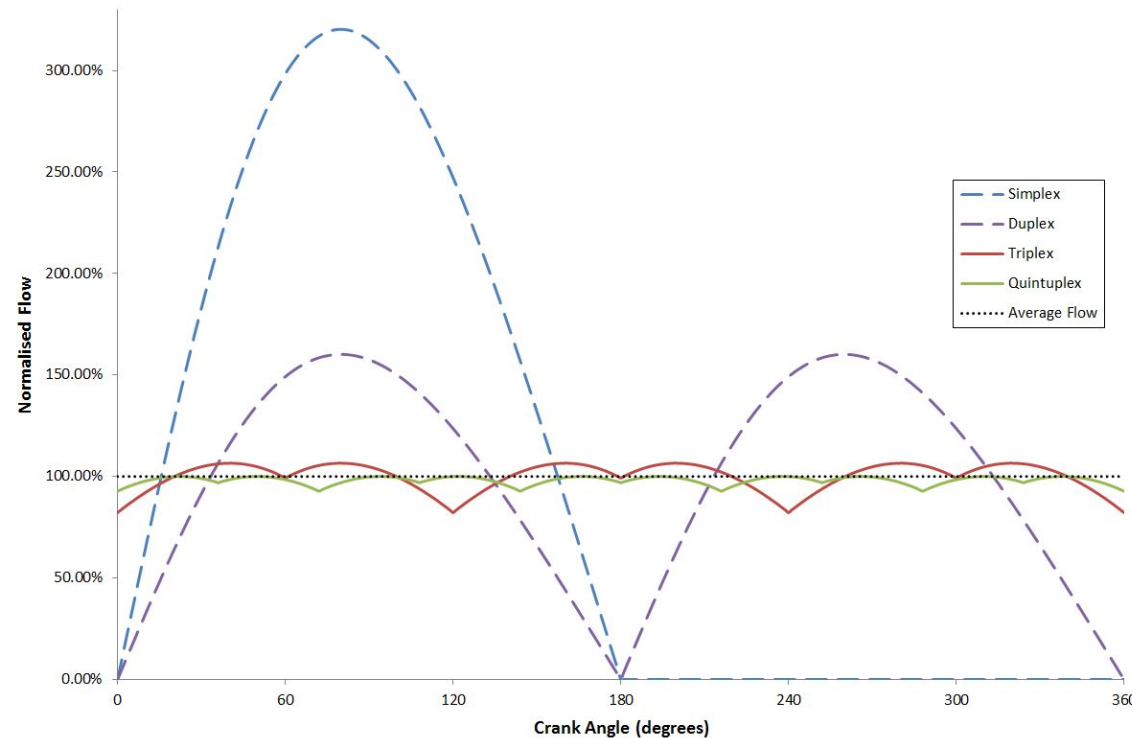
Name	No of Plungers
------	----------------

- | | |
|---------------------|----------|
| • Simplex | 1 |
| • Duplex | 2 |
| • Triplex | 3 |
| • Quintuplex | 5 |
| • Septuplex | 7 |



Reciprocating Pump Characteristics

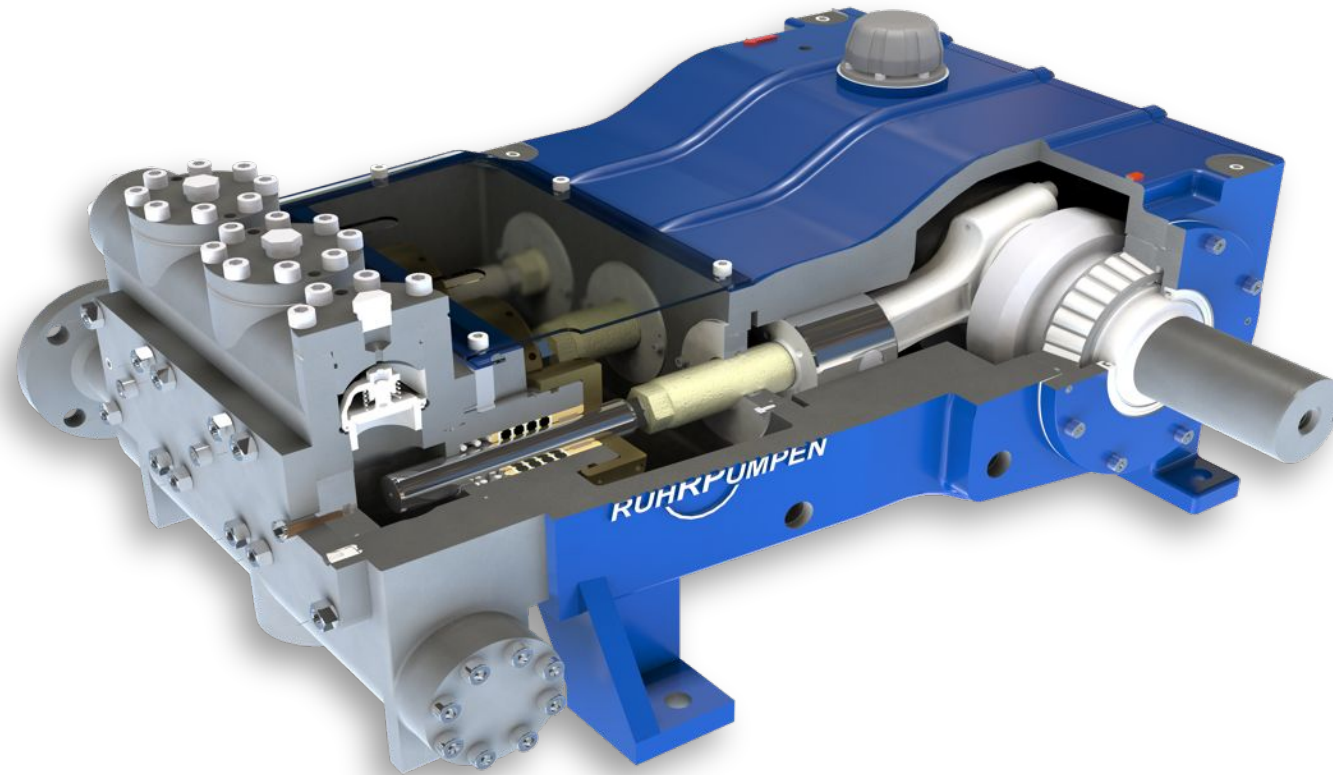
- Due to the nature of reciprocating pump action, flow pulses (unlike a centrifugal pump)
- The result is pulsations which are of different forms depending on number of plungers





Section 2 Part 3- RUHRPUMPEN RDP PUMP FEATURES

RUHRPUMPEN RDP PUMP



RDP Product Range & Nomenclature

Nomenclature :

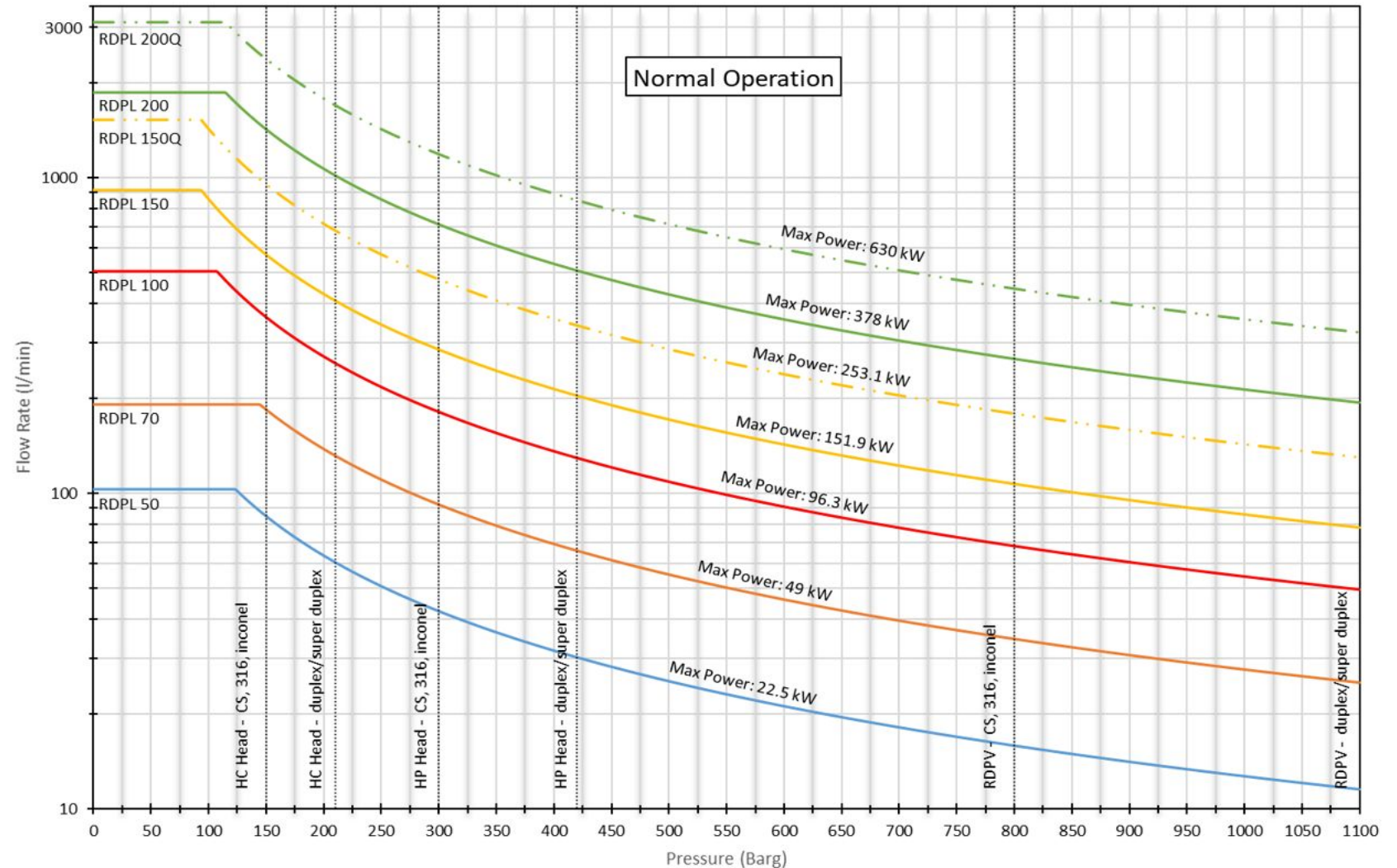
- Product name: RDP
- Suffix number: Stroke length
- Second number: plunger diameter
- Number of plungers: 3 (triplex) unless otherwise indicated by "Q" (quintuplex – 5 plungers)

Example:

RDP 100/55

Stroke length = 100 mm

Plunger diameter = 55 mm



The Balancing Act

Rod Load



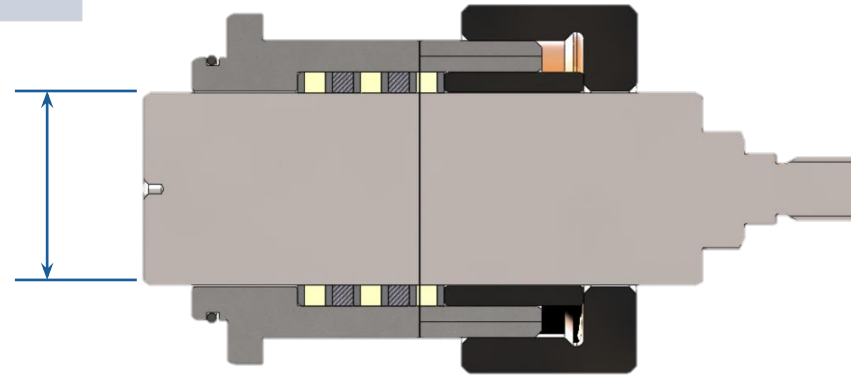
Speed
RPM

Plunger $\varnothing$

The Balancing Act

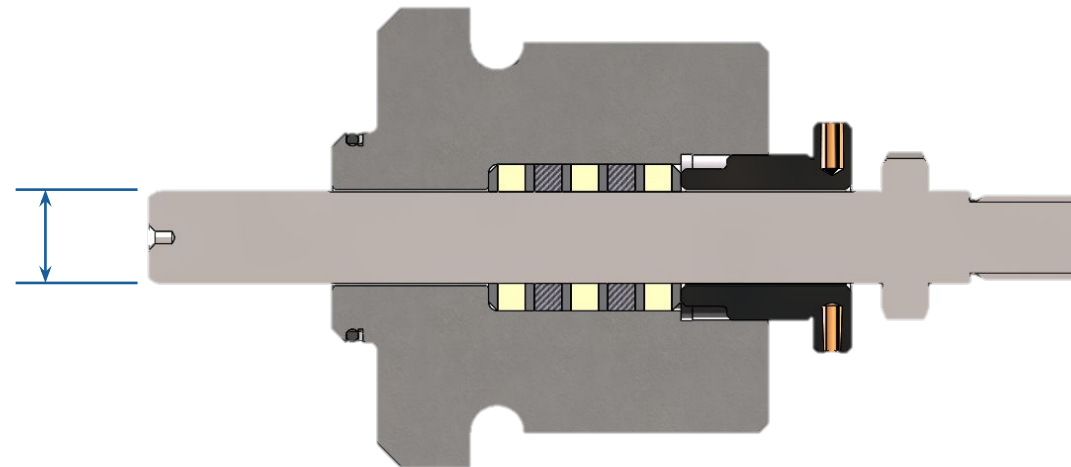
Pump Model	50	70	100	150	200
Max Rod Load Kg	3300	3500	5500	7500	15000

Ø 200mm
@ 47 bar
=1500 Kg

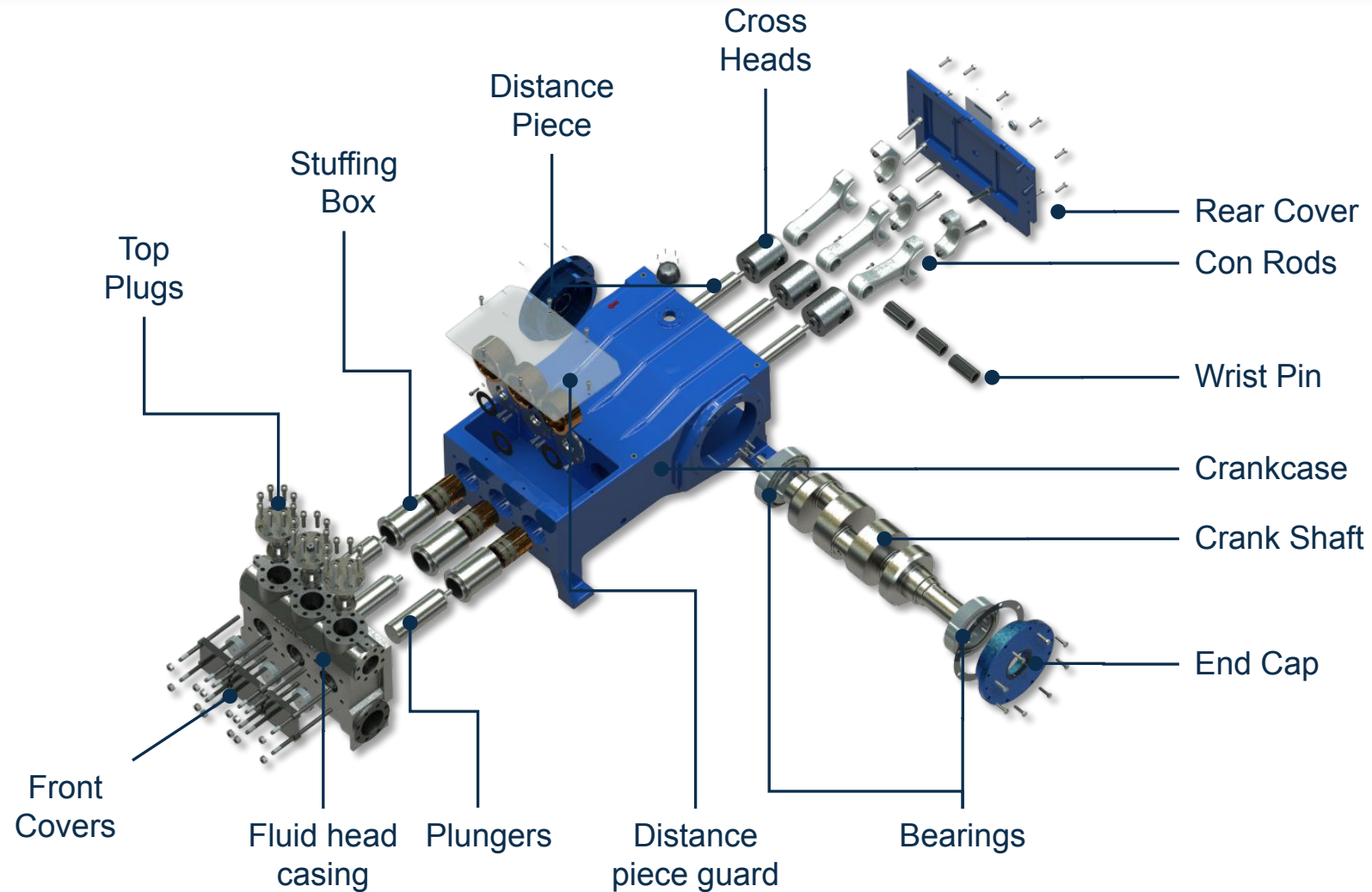


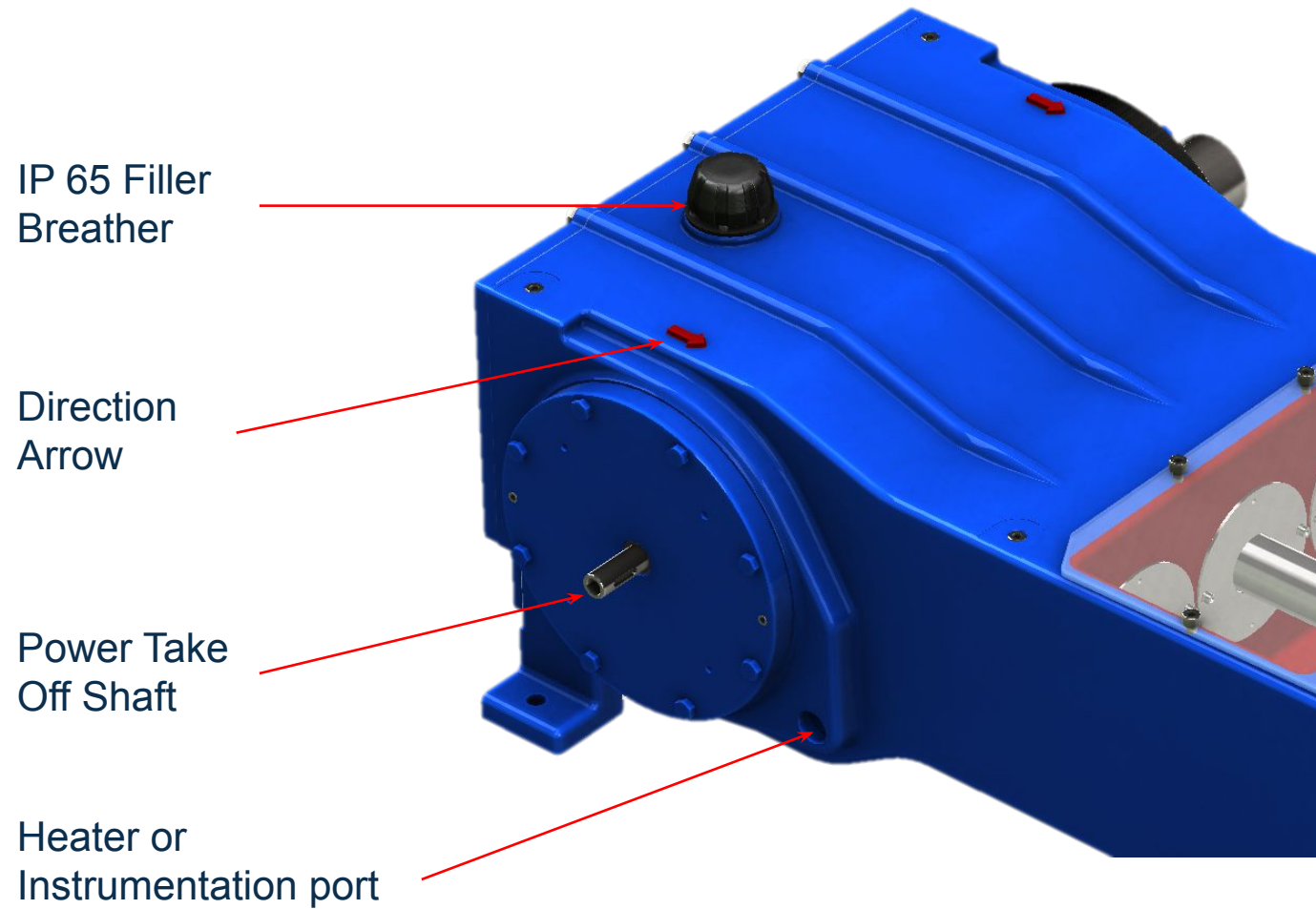
Force = Pressure x Area

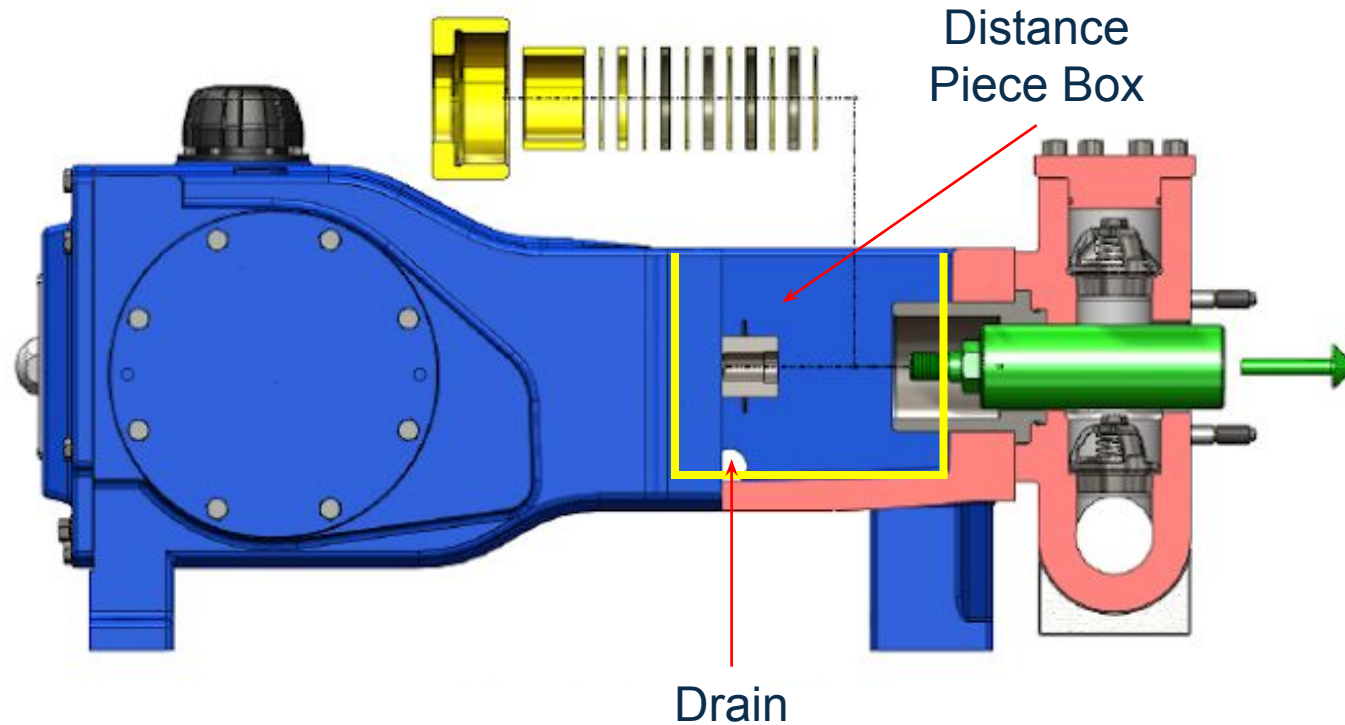
Ø 43mm
@ 1000 bar
=1500 Kg



Pump Assembly



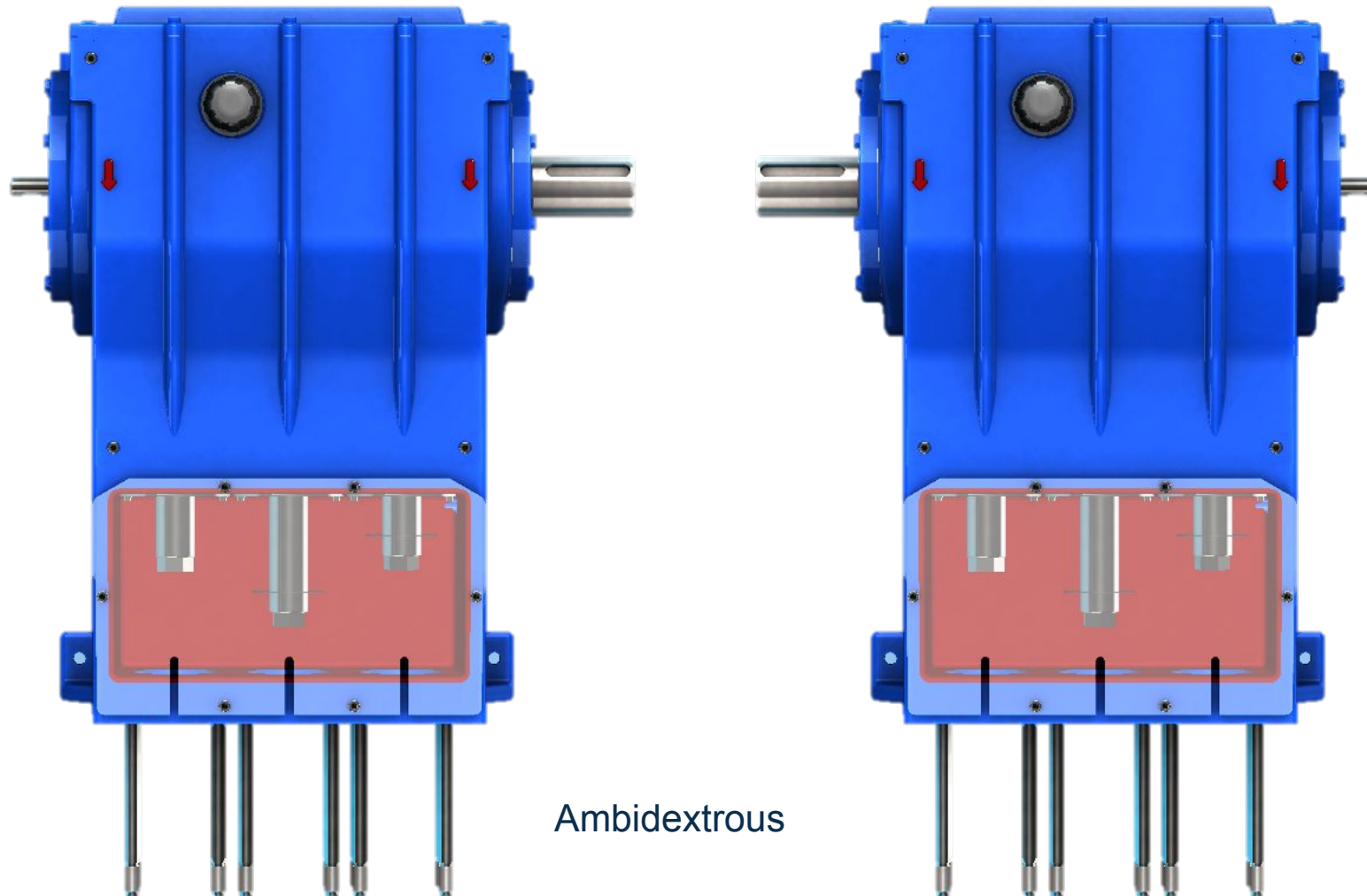




Distance Piece Box - an important maintenance feature – not all competitors have it

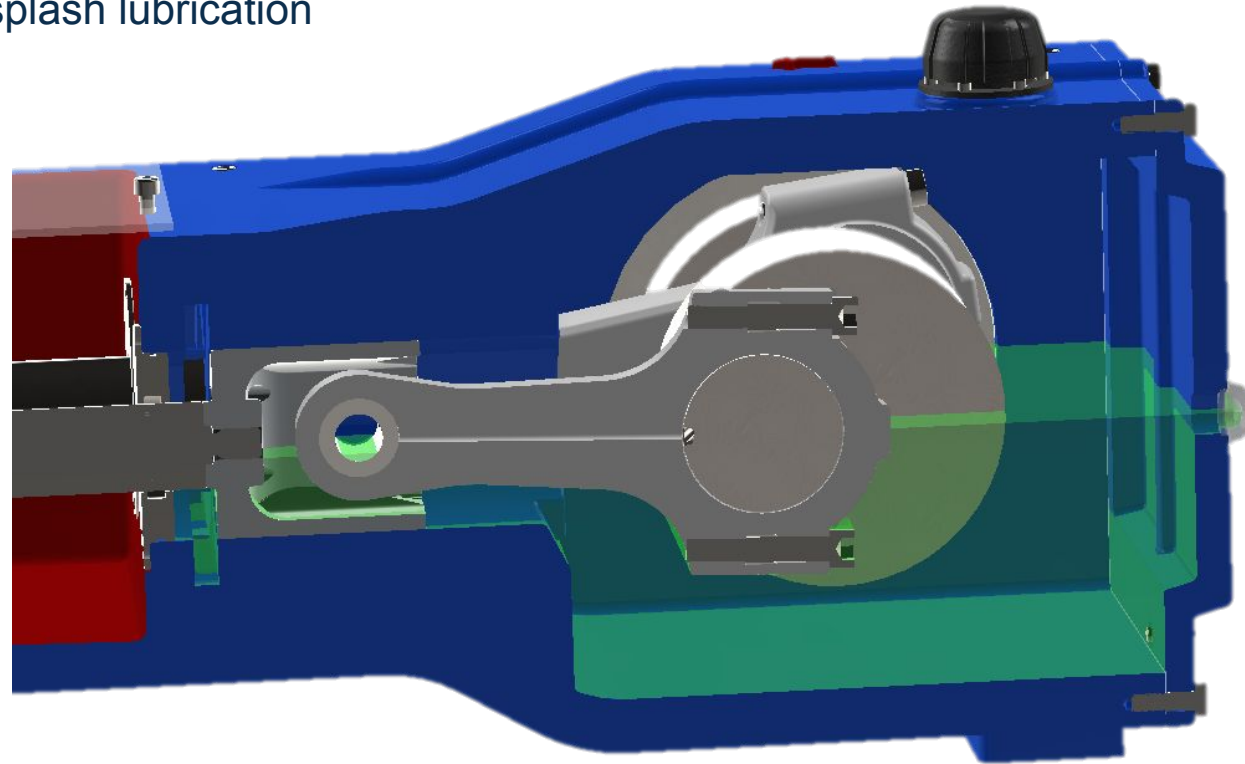
Permits piston and packing exchange without power end dis-assembly and other maintenance tasks (eg change oil lip seal) without disturbing fluid head end

Distance piece box can be used for containment of packing or oil leakage



Power End Lubrication Splash

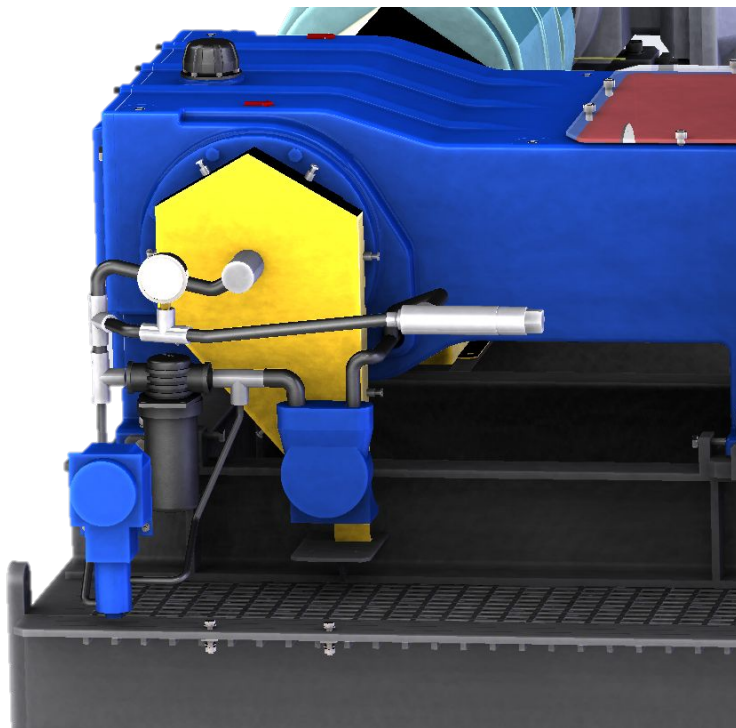
Flooded/splash lubrication



Power End Lubrication Forced

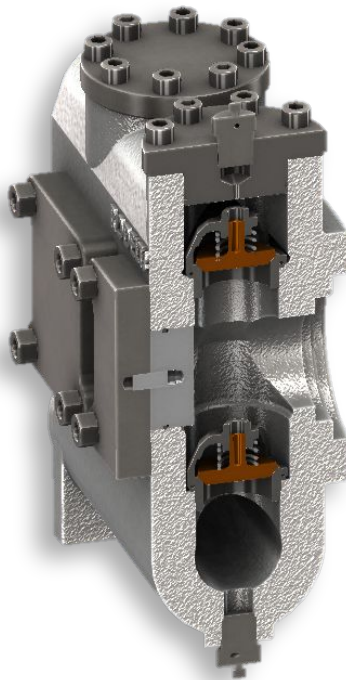
Optional forced feed lube system

Criteria based on inlet pressure and speed



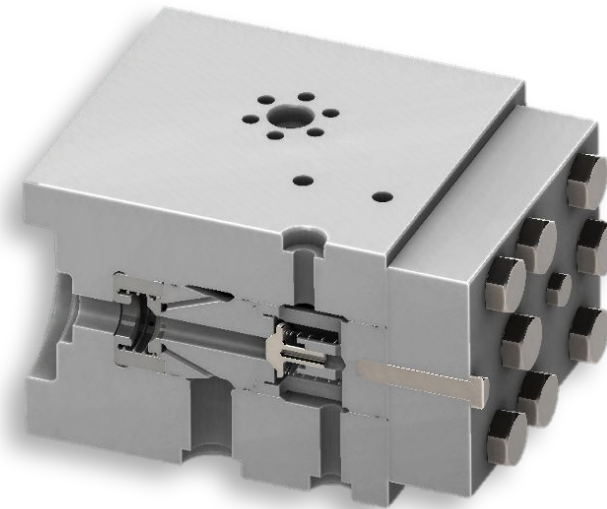
Fluid Head Types

Three types of head designations - Selection depends on material and pressure



HC High capacity
HP High pressure

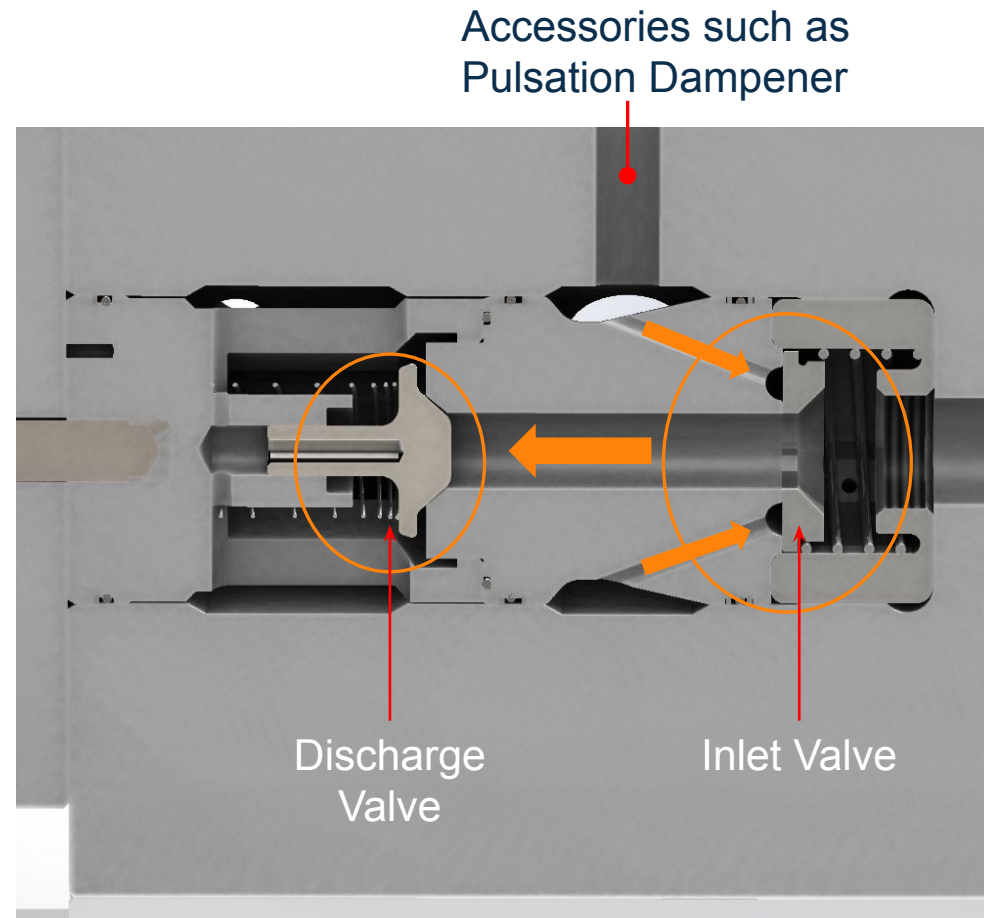
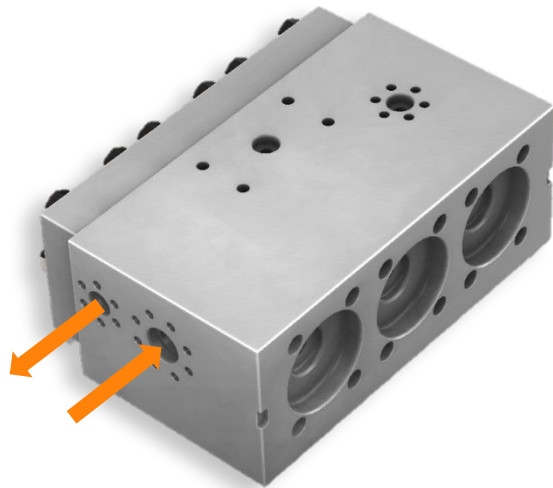
	HC	HP	VHP
Head Material	Max Pressure Bar g		
Carbon	150	300	950
316L	150	300	950
Duplex F53	250	500	1100
Super Duplex F55	250	500	1100
Inconel 625	250	500	1100



VHP Very high pressure

WHY IS VHP DIFFERENT?

Forged design



Valve Technology

Top Guided Bevel

- High stability for greater efficiency and lower noise

Tapered seats

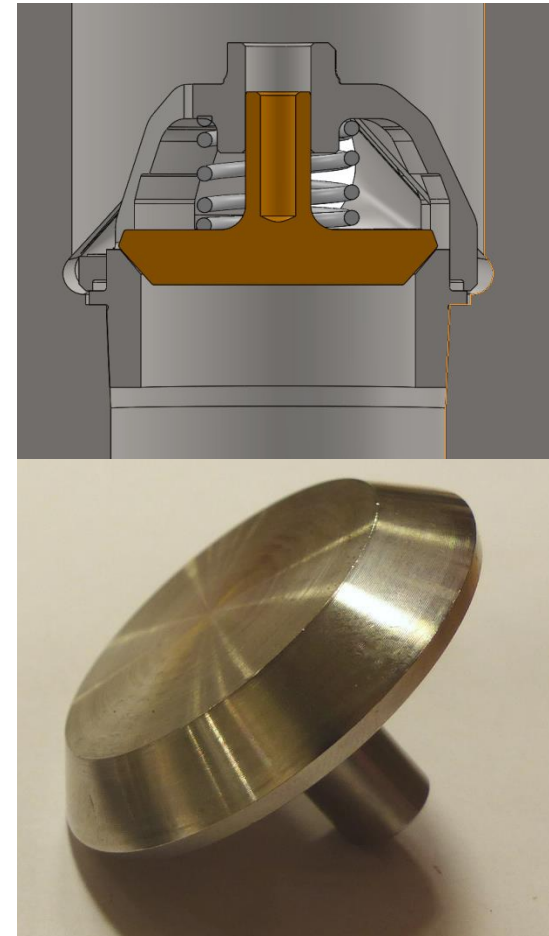
- For corrosion and erosion resistance

Ruhrpumpen proprietary valve gives us maximum flexibility from design and manufacturing standpoint

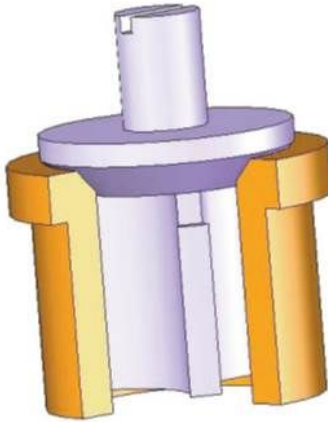
API 674: 6.7.3 Valve Seats

Valve seats shall be replaceable

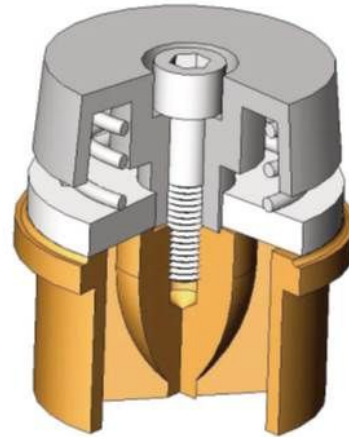
For corrosive service seats shall be pressed into tapers in the Head



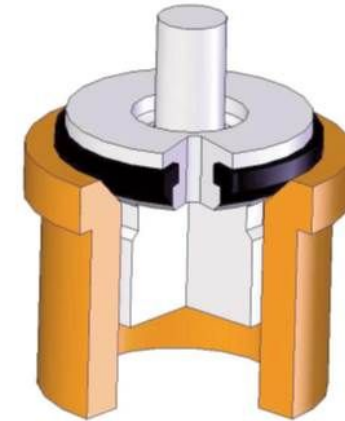
Typical Valve Types



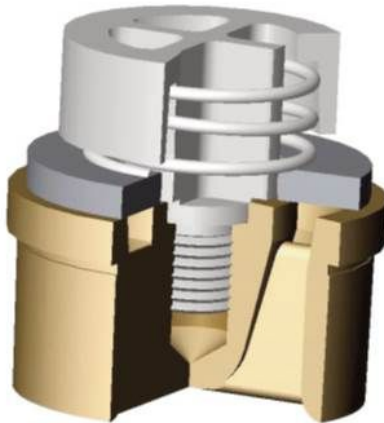
Wing Guided Bevel



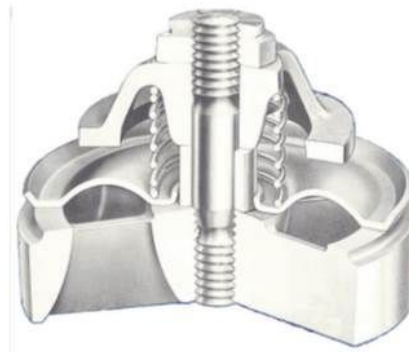
Disk Type, Centre Guided



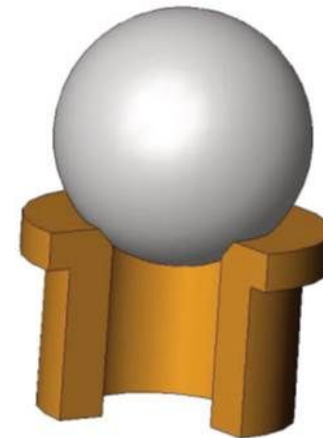
Wing Guided Bevel
Polymer Seal



Disk Type, Double ported



Durable Disk



Ball

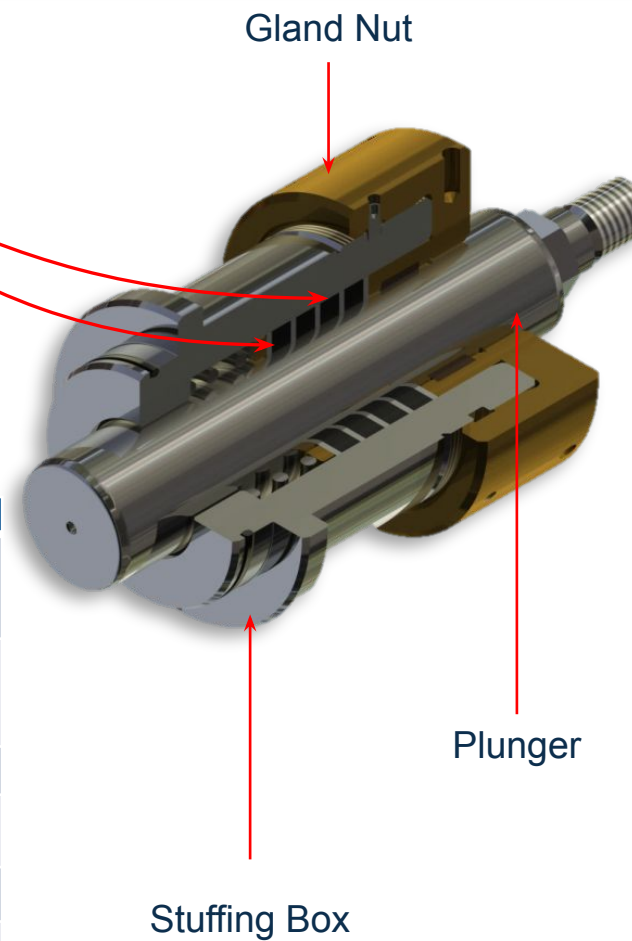
Plunger Sealing Assembly

Packing

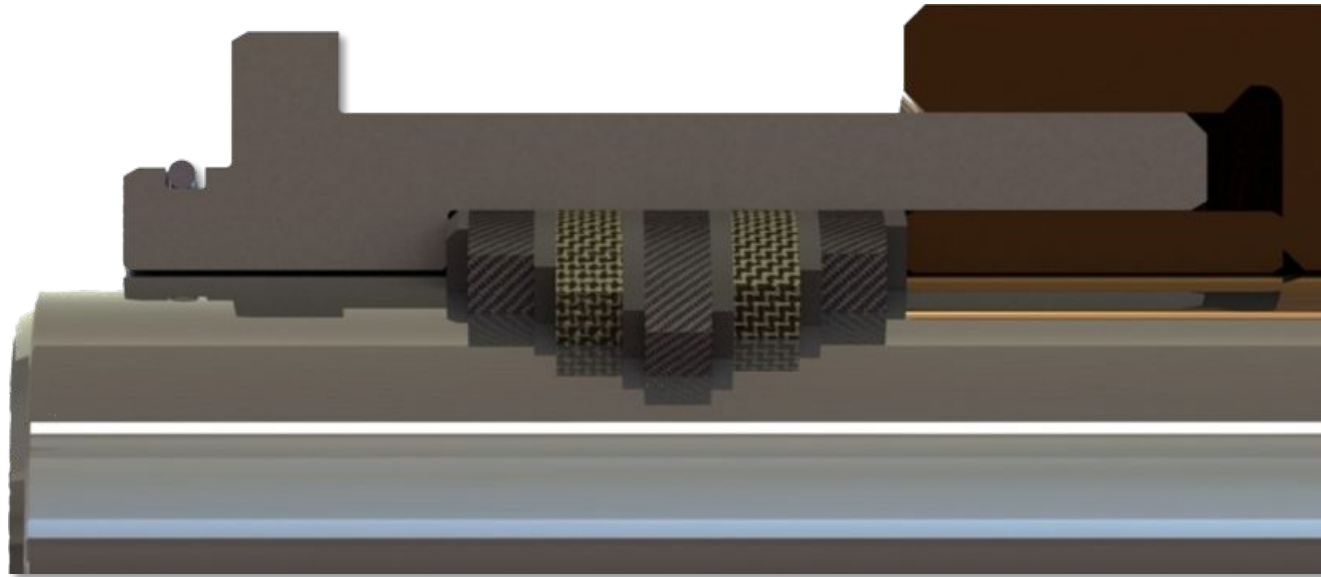
Type: Braided/Chevron
Adjustment: Manual/Sprung
Lubrication: Product or External

Typical Packing Example

Media	Seal System	Metallic parts	Packing
Caustic solution	Flushed Plan "62"	316	Braided
Closed Drain/ H2s present	Force feed lube sprung loaded Packing	Duplex	Sprung Chevron
Methanol	Force feed lube	316	Braided
Sea Water (RO)	Flushed Plan"13"	Super Duplex	Chevron (Single)
Meg/TEG	Standard 5	316	Braided
Hydrocarbons	Standard 5 OR Force feed lube	316	Braided



Stuffing Box Braided Compression Packing

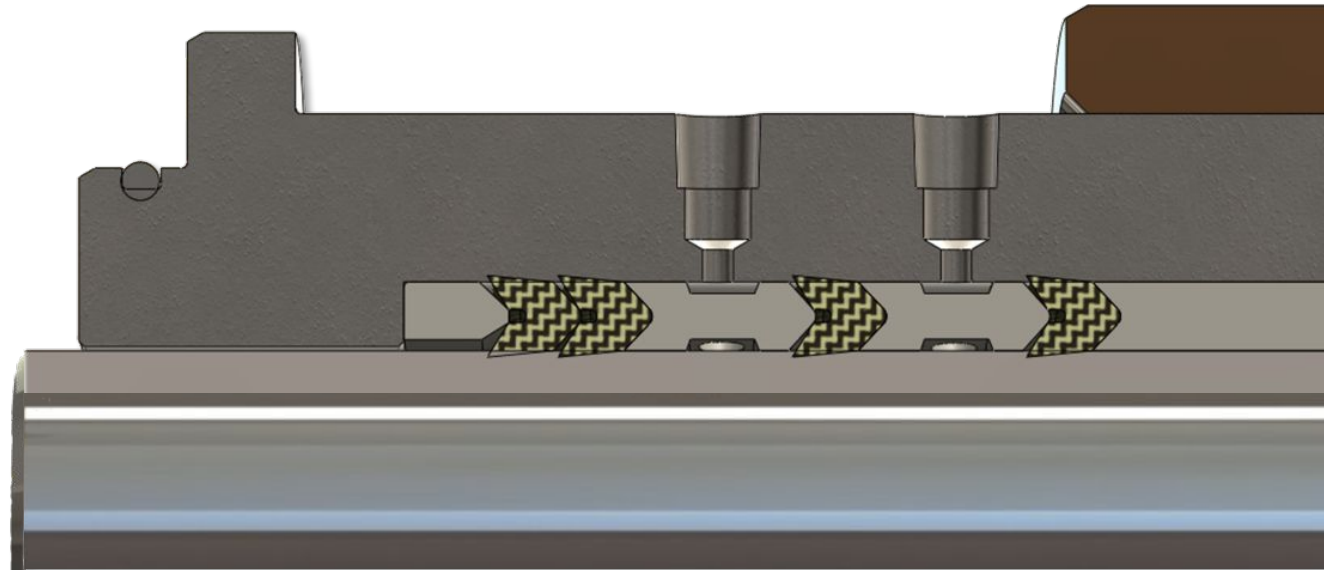


Standard 5 Layout

- 3 PTFE & graphite braided
- 2 PTFE & graphite & aramid braided
- 6 anti extrusion rings
- Simple and effective
- Requires regular manual adjustment



Stuffing Box Chevron Ring



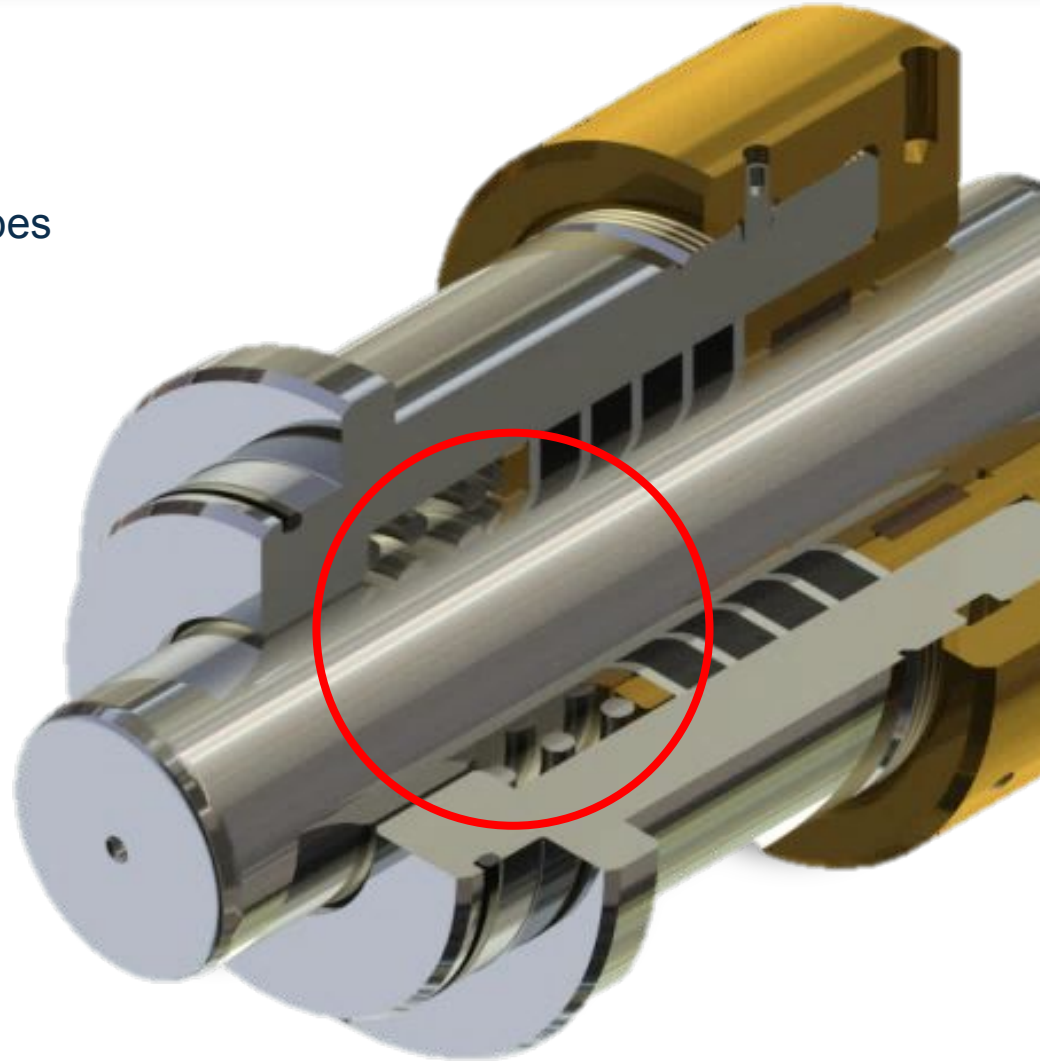
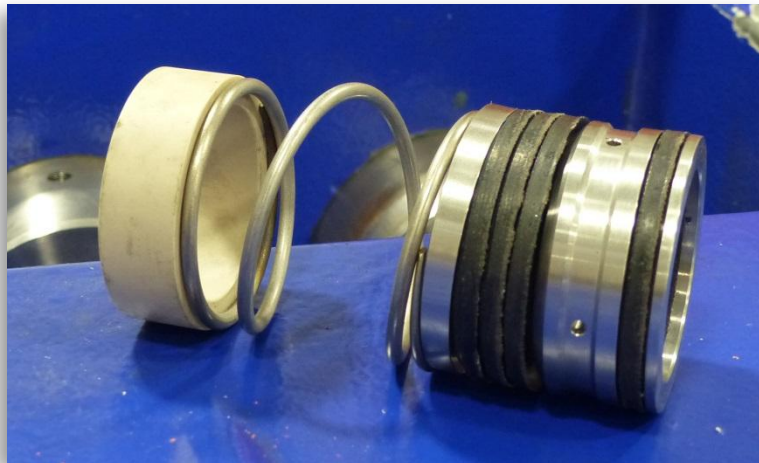
- Multiple packing rings
- Rings are one piece without a break
- No anti extrusion rings
- Little adjusting required
- Fewer parts
- Limited standard sizes



Stuffing Box Spring Loading

Single spring to preload packing

Can be used with Braided or Chevron types



Lubrication For Seal Life / For Emission Control

Product Lubrication

Media migrates along packing providing cooling and lubrication between packing and plunger

Flushing

Shop or grey water flushed, by mains pressure, auxiliary pump, gravity or suction line

- Cools packing

- Flushes particulates

- Prevents crystallisation or coking (similar to Plan 62)

- With Reverse Osmosis water is taken from the suction line to flush and cool the rear of the seal (Similar to Plan 13)

- Only single feed

- Used with braided or chevron packing

Forced Feed for Lubrication/Cooling

Compatible fluid is pressure fed into the packing by an auxiliary pump driven via power take off shaft extending from the pump crankshaft

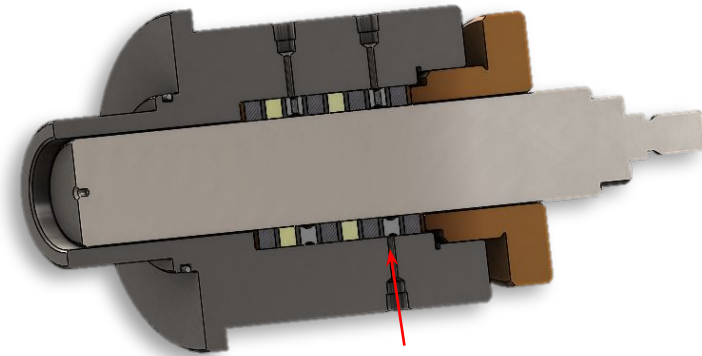
- Used with low lubricity solvents e.g. methanol

- Single or double feed

- Used with braided or chevron packing

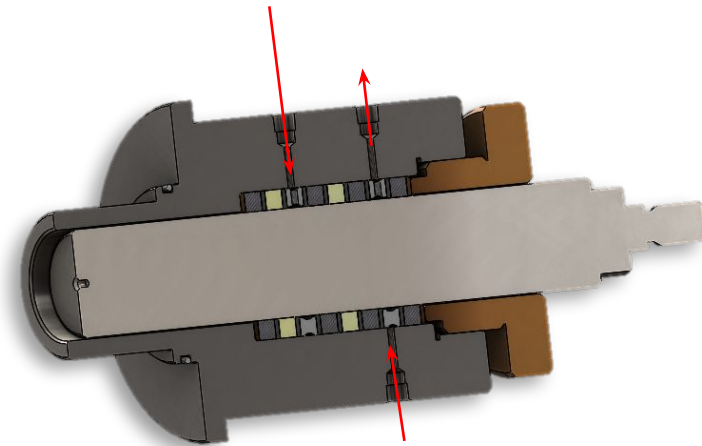
Forced Feed for Emission Control

Used as a barrier with high toxic media such as closed drains containing H₂S.



Front Lube:
Discharge Pressure + 5 bar

Back Flush

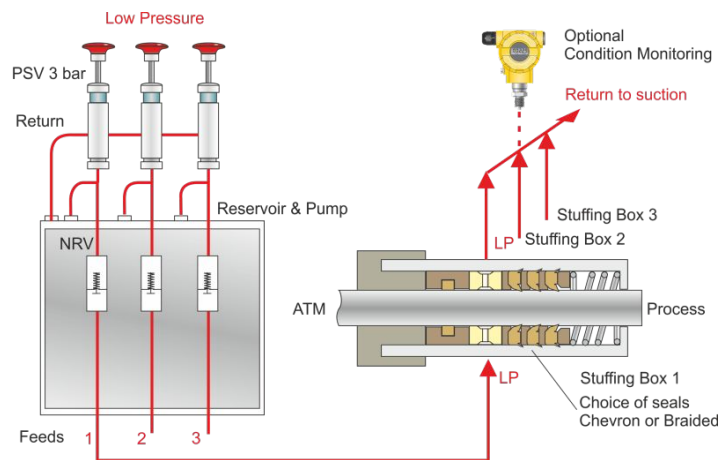


Back Lube:
Pressure 3 / 5 Bar

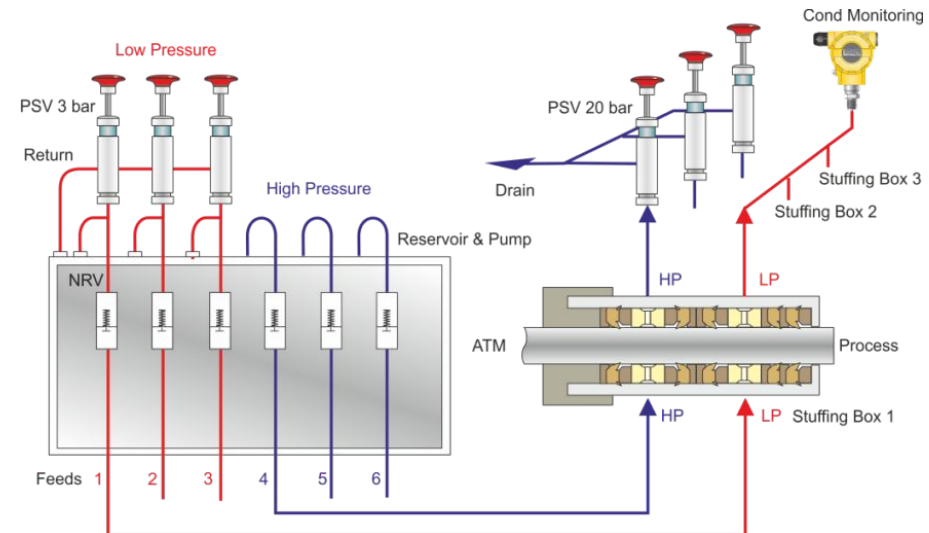
Lubrication For Seal Life / For Emission Control

TYPICAL System schematics

TYPICAL 3 FEED SYSTEM



TYPICAL 6 FEED SYSTEM



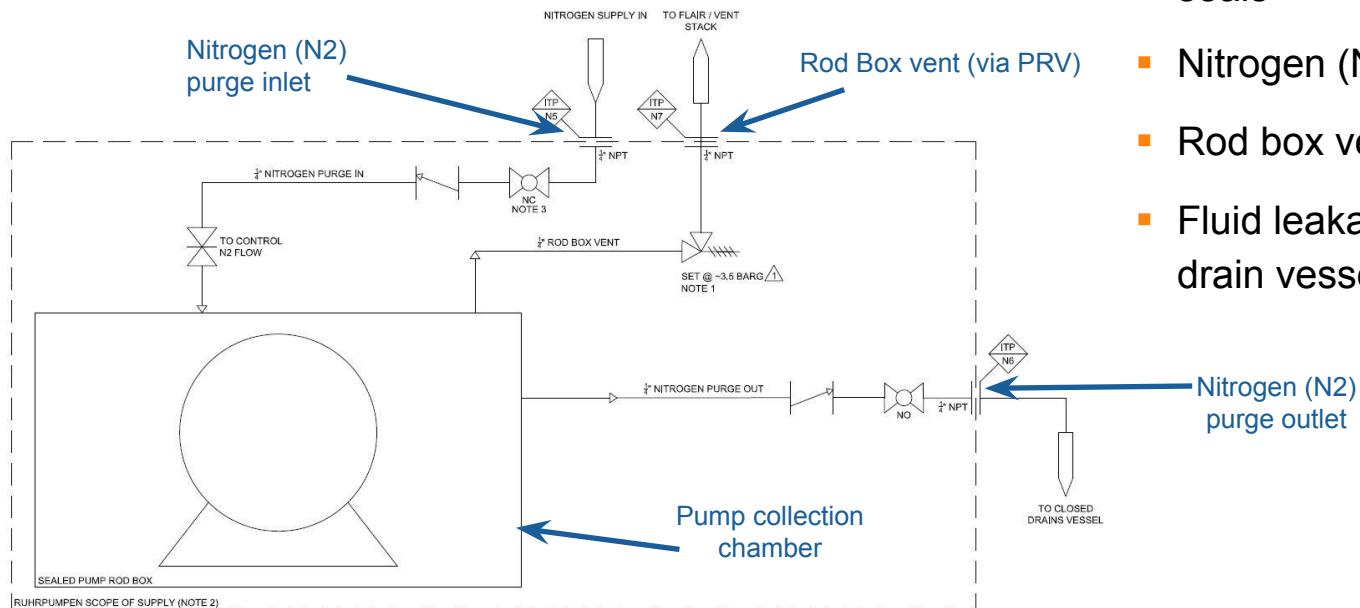
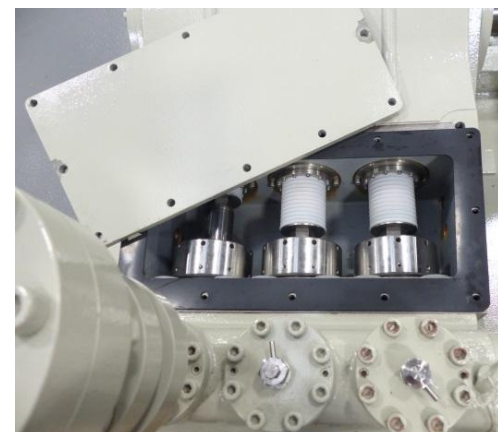
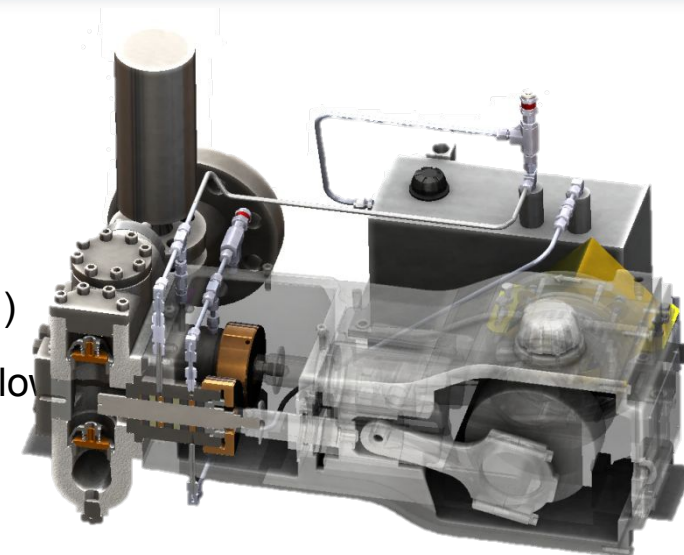
Sealed Rod Box

WHEN TO BE USED:

- In addition to stuffing box sealing systems
- To prevent uncontrolled release of toxic or hazardous **gases** contained in pumped media

HOW IT WORKS

- Gas tight sealed distance piece chamber (access cover is vented)
- Gas tight connecting rod with bellows seals
- Nitrogen (N₂) inlet
- Rod box vent (via PRV)
- Fluid leakage outlet (to a closed drain vessel)



API674 reciprocating pumps do not use seal plans in the same sense as centrifugal products

BUT...

There are some parallels with recognised API 682 seal plans. See table

Title	Similar API682 Plan	Application	Construction	How it works
Standard (Non Lubricated)	-	No concern about duty or media such as toxicity or lubrication.	Comprises a primary seal stack with no seal plan.	-
Forced Lubrication (3 Feed)	-	Media unable to lubricate the seals sufficiently Also used in high pressure and speed applications.	Comprises primary and secondary (unloaded) seal stacks separated by a lantern ring. A Mechanical Lubricator injects low pressure oil into the Lantern Ring to lubricate the seals.	Mineral oil is injected into the lantern ring chamber. Exploiting surface imperfections oil migrates along the plunger. During the suction stroke the packing relaxes and lubricant is drawn into contacting surfaces.
Barrier Fluid	53	RESTRICTS fugitive emissions of toxic media.	Comprises primary, secondary (loaded) and tertiary (unloaded) seal stacks separated by lantern rings. Barrier fluid is circulated through the first lantern ring at a higher pressure than discharge. Barrier fluid will be compatible with the pumped media.	Barrier fluid injection pressure is higher than the discharge stroke. Consequently barrier fluid migrates across the seals towards the front of the stuffing box rather than the rear, thus blocking media escape. Packing condition is critical to this process.
Sealed Rod Box	-	BLOCKS fugitive emissions of toxic media.	The Distance Piece Chamber (containing the stuffing boxes) features a solid metal cover. A gastight gasket with 'O' rings and Flexiseals prevent any media escape to atmosphere. PSV, drain and nitrogen purge connections are provided. Any accumulated fluid leakage is detected by level switch	By sealing the Distance Piece Chamber with static seals ALL gaseous and fluid emissions that occur from the stuffing boxes are fully contained. Any fluid leakage is safely collected and safely piped to plant disposal. A Nitrogen purge facility removes toxic media prior to maintenance.
Return to Suction	13	Directs main leakage to suction where fugitive emissions are of no concern. Also used to feed lubrication to primary seals.	Comprises primary and secondary (unloaded) seal stacks separated by a Lantern Ring. Any leakage escaping the primary seal returns back to suction via the Lantern Ring. A check valve prevents back flow.	Any leakage that migrates past the primary seal stack collects in the lantern ring chamber. As the leakage pressure builds up it relieves into the suction line.

API674 reciprocating pumps do not use seal plans in the same sense as centrifugal products

BUT...

There are some parallels with recognised API 682 seal plans. See table

Title	Similar API682 Plan	Application	Construction	How it works
Packing Monitoring	65	Used where packing integrity is critical to reduce emissions. For predictive maintenance in remote applications and/or trigger safe shutdown	Comprises a primary and secondary (unloaded) seal stacks separated by a Lantern Ring. Any leakage escaping the primary seal enters the Lantern Ring and is directed to a drain line. Instruments in this line monitor/report the leakage flow rate.	Should the packing leakage flow rate increase beyond an acceptable level an alert is triggered to indicate that the primary seals are worn and require replacement.
External Flush	32	Media may crystallise where it leaks from the stuffing box.	Comprises primary and secondary (unloaded) seal stacks separated by a Lantern Ring. Clean (plant sourced) media is directed through the Lantern Ring to flush the Stuffing Box, the system includes inlet and discharge connections.	Clean media (normally non saline water) is injected into the Lantern Ring chamber with a high flow rate. Any media migrating past the primary seals is diluted and carried to the discharge of the flush.
Seal Heating/Cooling	-	Cooling: Protects seals in high temperature applications. Reduces cavitation risk of near gas media. Heating: Protects seals in cryogenic applications. Reduces risk of media solidifying.	Comprises a sleeve installed around the stuffing boxes with galleries to accommodate heating/cooling fluid. The system includes Inlet and discharge connections only. External closed loop system and/or heat exchanger are excluded.	Heating/cooling fluid is introduced into the sleeve with a certain flow rate to provide the appropriate heat transfer.
Discharge Flush (piped externally)	11	Used to decrease seal leakage.	Comprises primary and secondary (unloaded) seal stack separated by a Lantern Ring. External piping directs a small amount of discharge media to the Lantern Ring.	Use of primary and secondary seals reduces leakage. The flush from discharge provides extra lubrication and cooling to the secondary seals increasing reliability.
Discharge Flush (Internal galleries)	01	As above but internal galleries easier to heat in cold ambient temperature conditions.	Comprises primary and secondary (unloaded) seal stack separated by a Lantern Ring. Internal galleries direct a small amount of discharge media to the Lantern Ring.	Same as above.

Meets API 674 (ISO13710) Latest 3rd edition - One of first Pumps to do so

Simple configurable design

ATEX Compliance – Ex c (constructional safety) Ex cb (control of ignition sources)

Excellent noise characteristics

- Less than 85 dB (A) can be achieved

Low cost of ownership

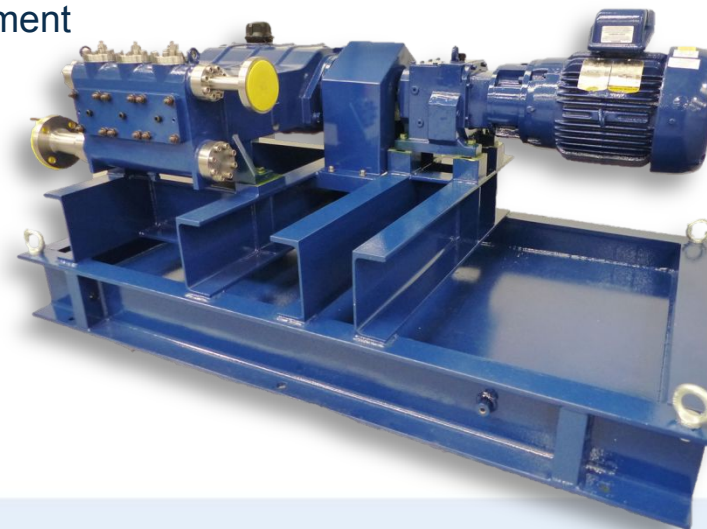
- In situ servicing of major parts without disturbing plant pipework
- Extended life – Greater wear allowances offer refurbishment
- Extended service intervals for all wear parts

Can meet diverse Oil Industry specifications

- NACE MR01-75, Norsok, Shell ES135, GOST R, GOST K, GGTN

Efficiency meets/exceeds API requirements

- 95% Volumetric
- 90% Mechanical





Section 2 Part 4- TESTING

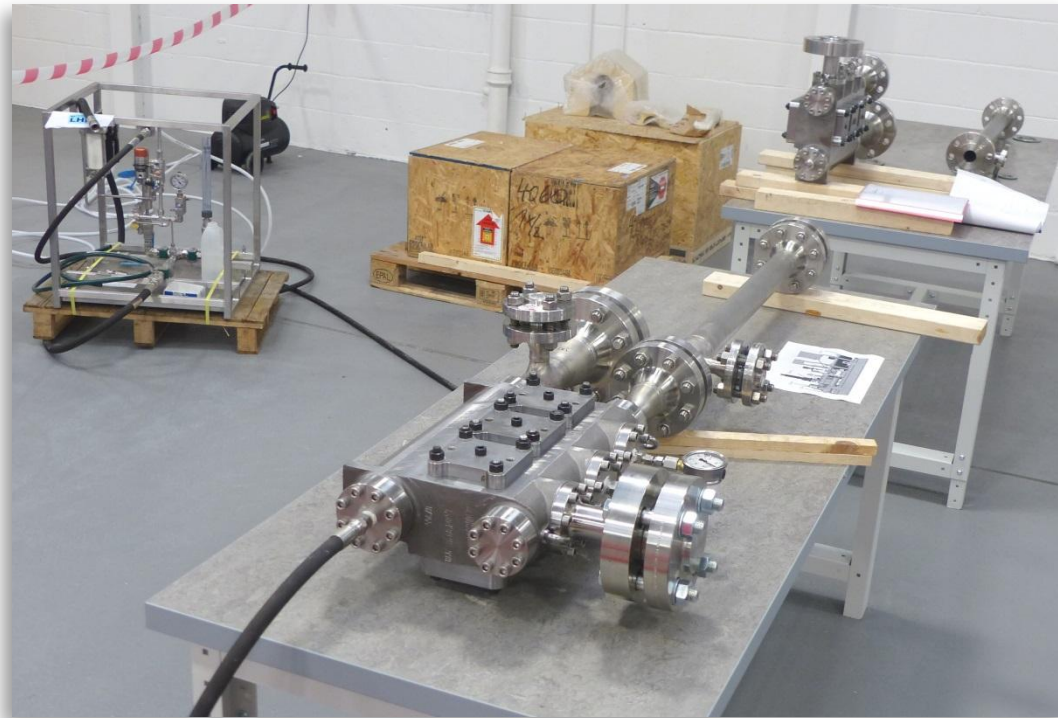
All the normal NDT

- Hydro test
- Mechanical running
- Performance
- Noise
- NPSH



1.5 x maximum pressure

Minimum of 30 minutes for API 674



Performance Test

Run at rated pressure and flow

Data taken at different
times to ensure repeatability

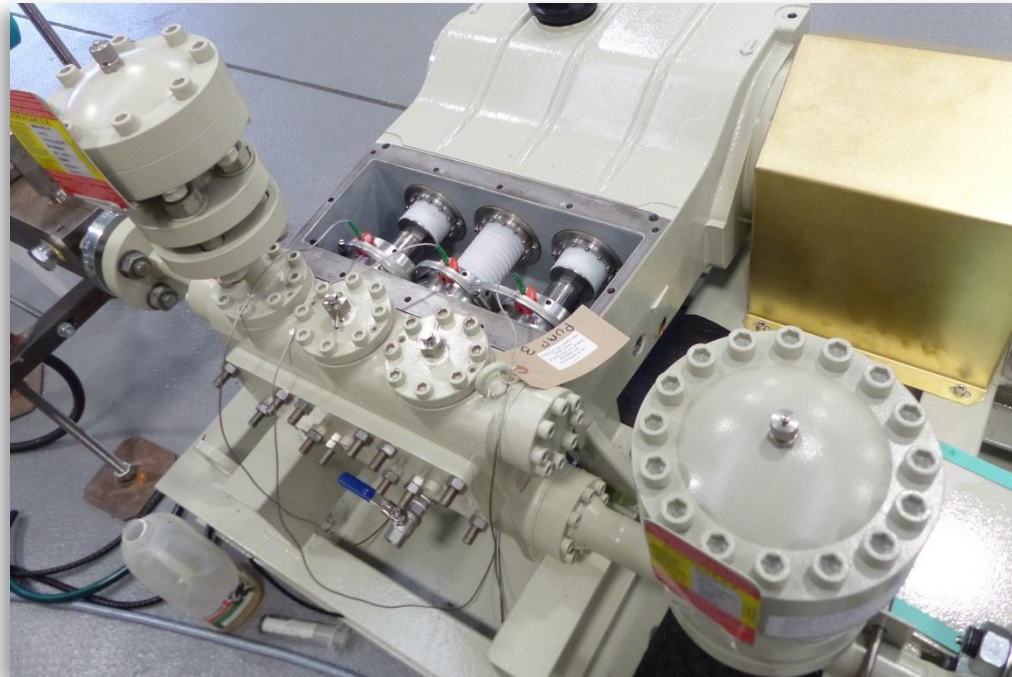
Parameter	Tolerance
Rated capacity	$+\leq 3\%$, -0%
Rated power	$+\leq 4\%$



Mechanical Running Test

Four hours at rated flow
Record temperatures:

- Stuffing box
- Power end bearings
- Gearbox



NPIP test

- Pressure plot upstream of any device used to improve inlet flow (pulsation dampener) and compared with the P_v of pumped fluid.
- Acceptance criteria:
 1. pressure spikes with peaks $< 300\%$ of average inlet pressure
OR
 2. pressure spikes with peaks $< 110\% P_v$

NPSH test

- Reduce system NPSHA until 3% drop in flow is seen
- This point defines the NPSHR of the pump

NOTE : Only one of the two tests is required.



RDP 70 Pump on Test





Section 2 Part 5- PACKAGE OPTIONS AND AUXILIARIES

•Transmission

- Gear box
- Drive belt
- Hydraulic

•Motor

- Electric
- Diesel
- Petrol
- Hydraulic
- Turbine

•Drives

- Variable Speed Drive (VFD)
- Soft Start

•Dampeners / PSV

- Loose
- Fitted

•Transmission Guard

- Material Selection

•Transmission Coupling

- Close coupled
- Spacer
- Direct

•Base Frame

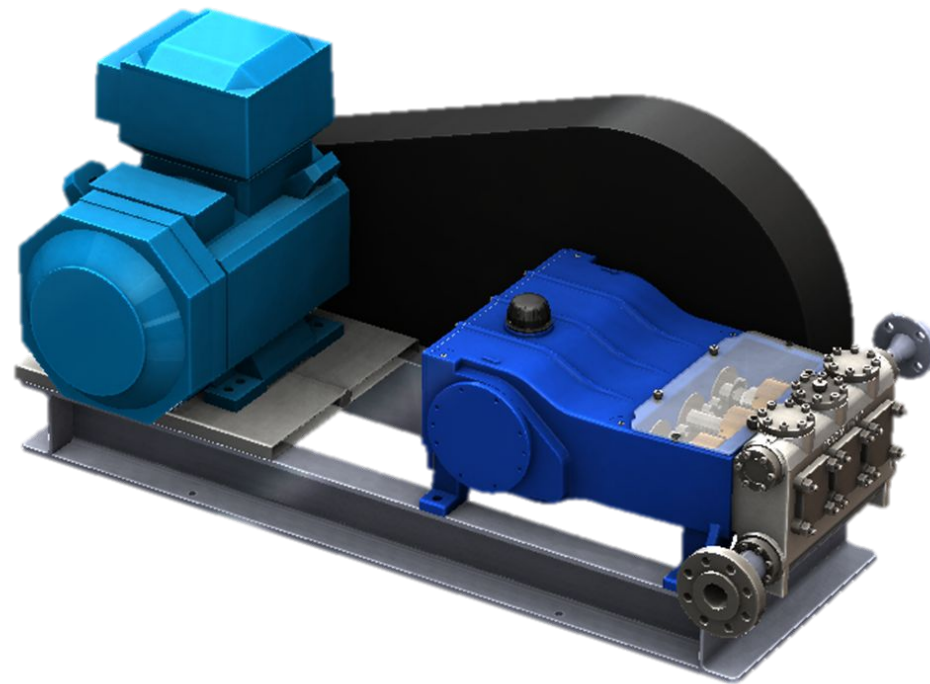
- Jacking pads
- Grouting
- Drip tray
- Grating
- Earth bonding

•ATEX

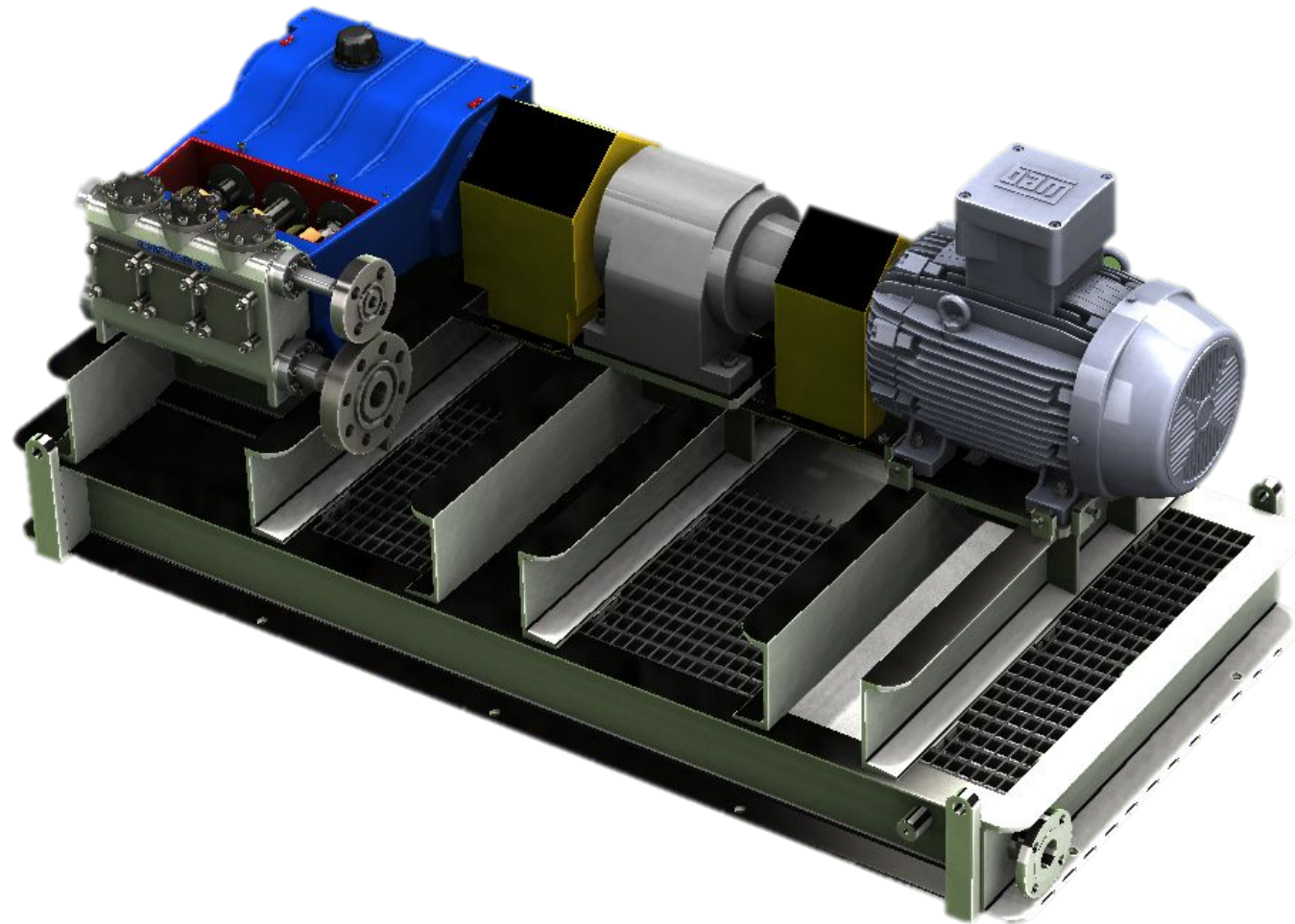
- Ex c
- Ec cb

•Monitoring equipment

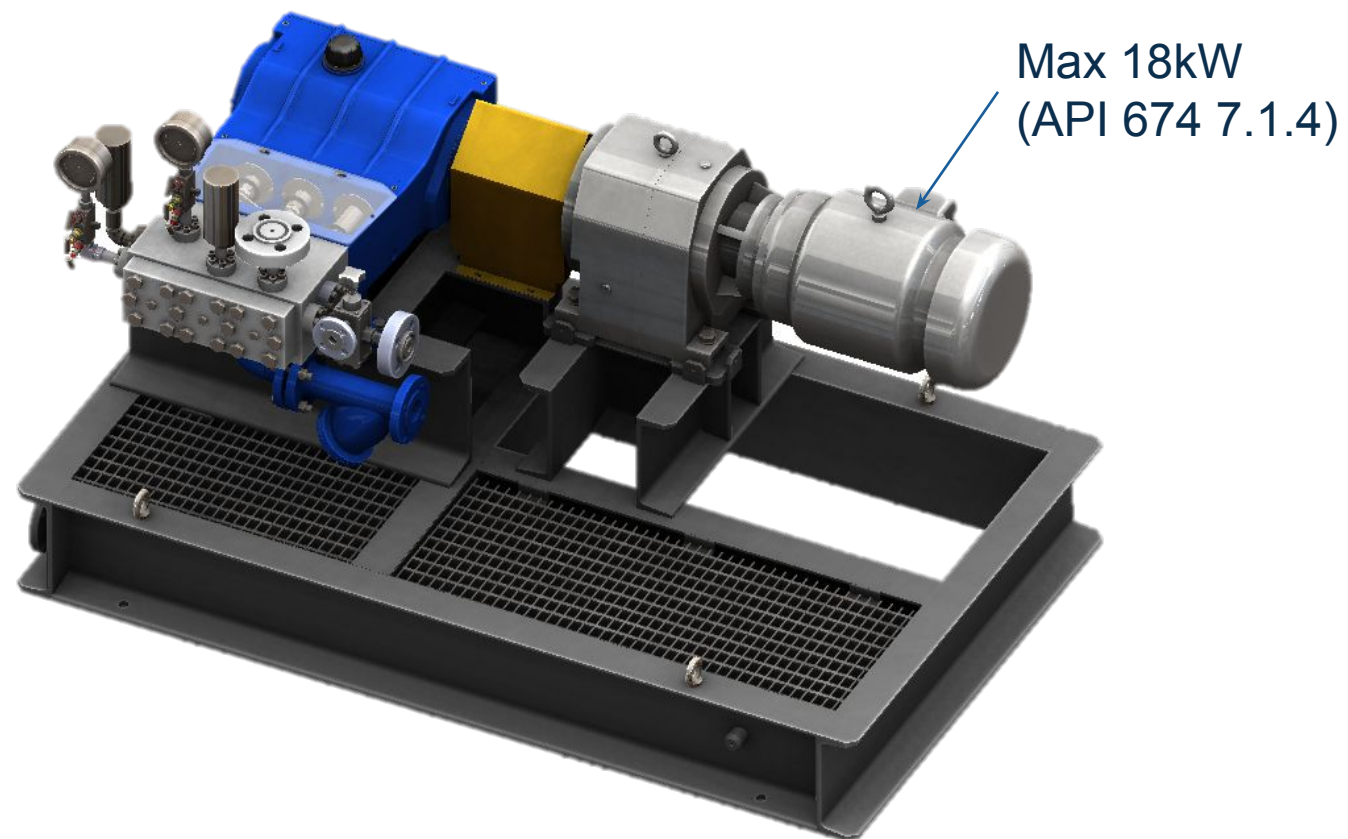
Belt Drive



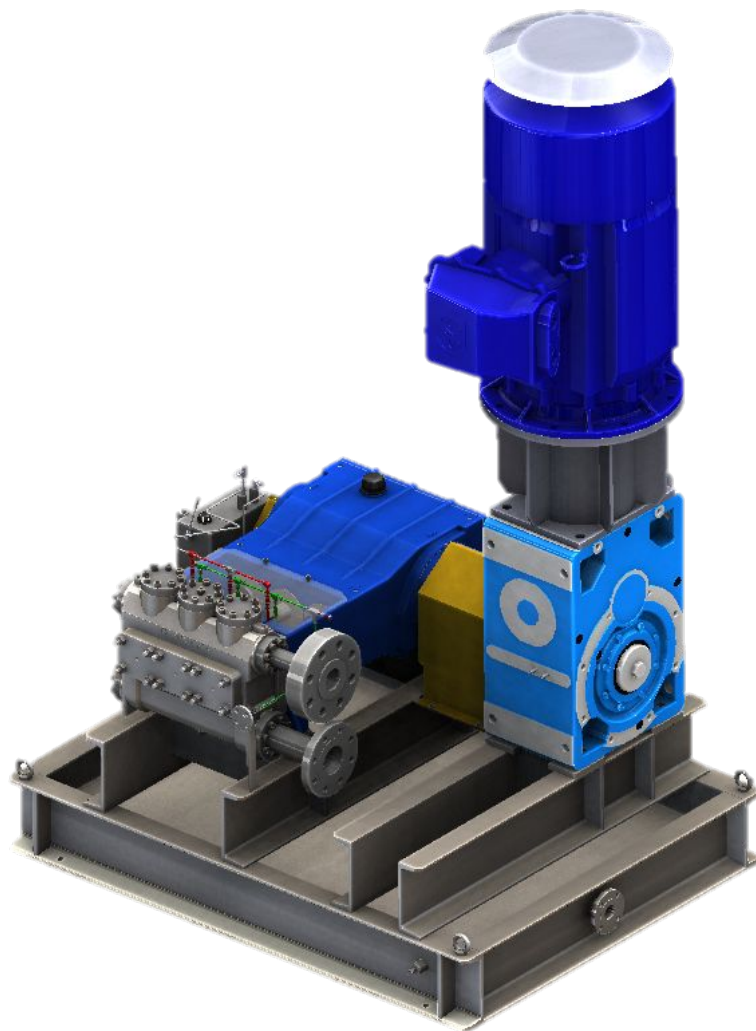
Gearbox Drive



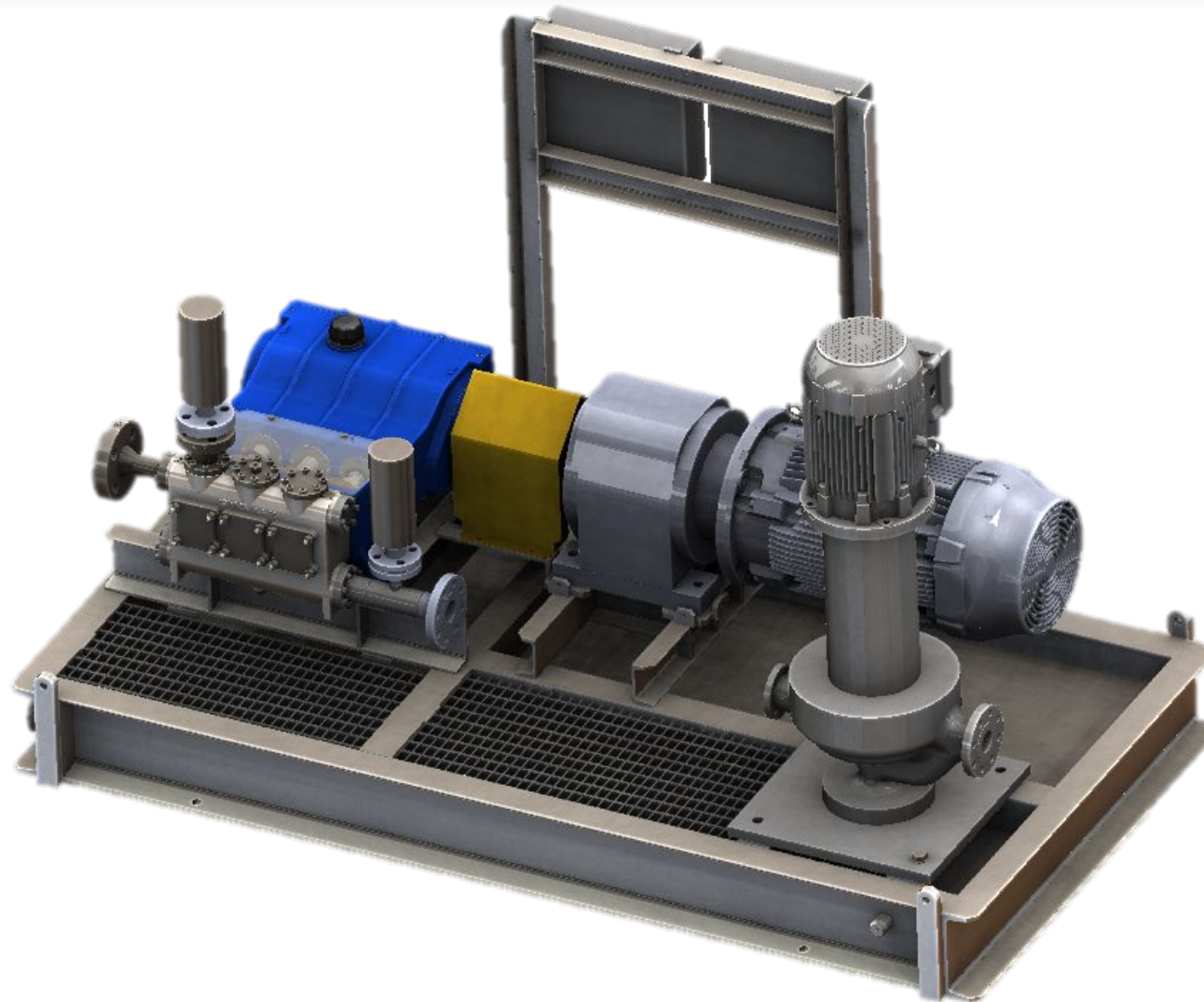
Gearbox Direct Drive



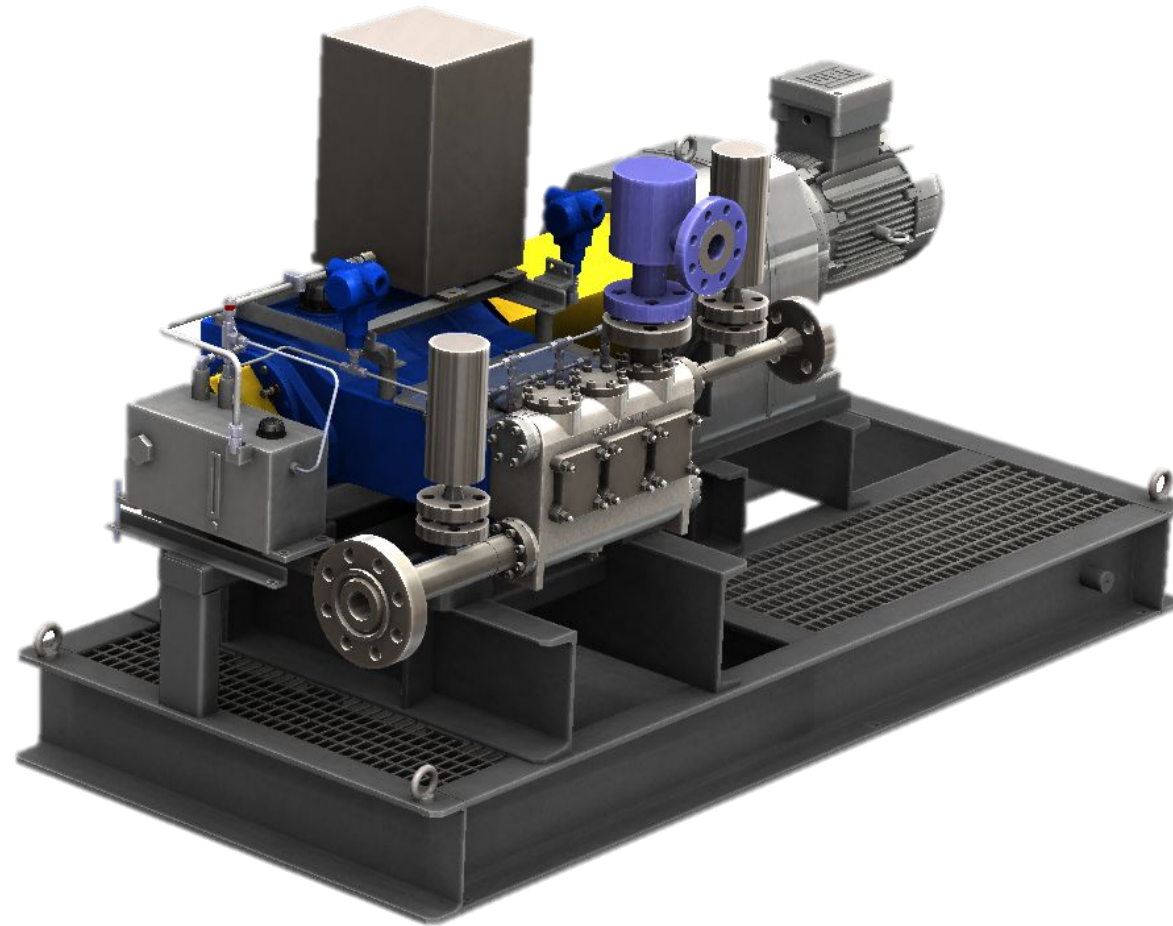
Gearbox Vertical Drive



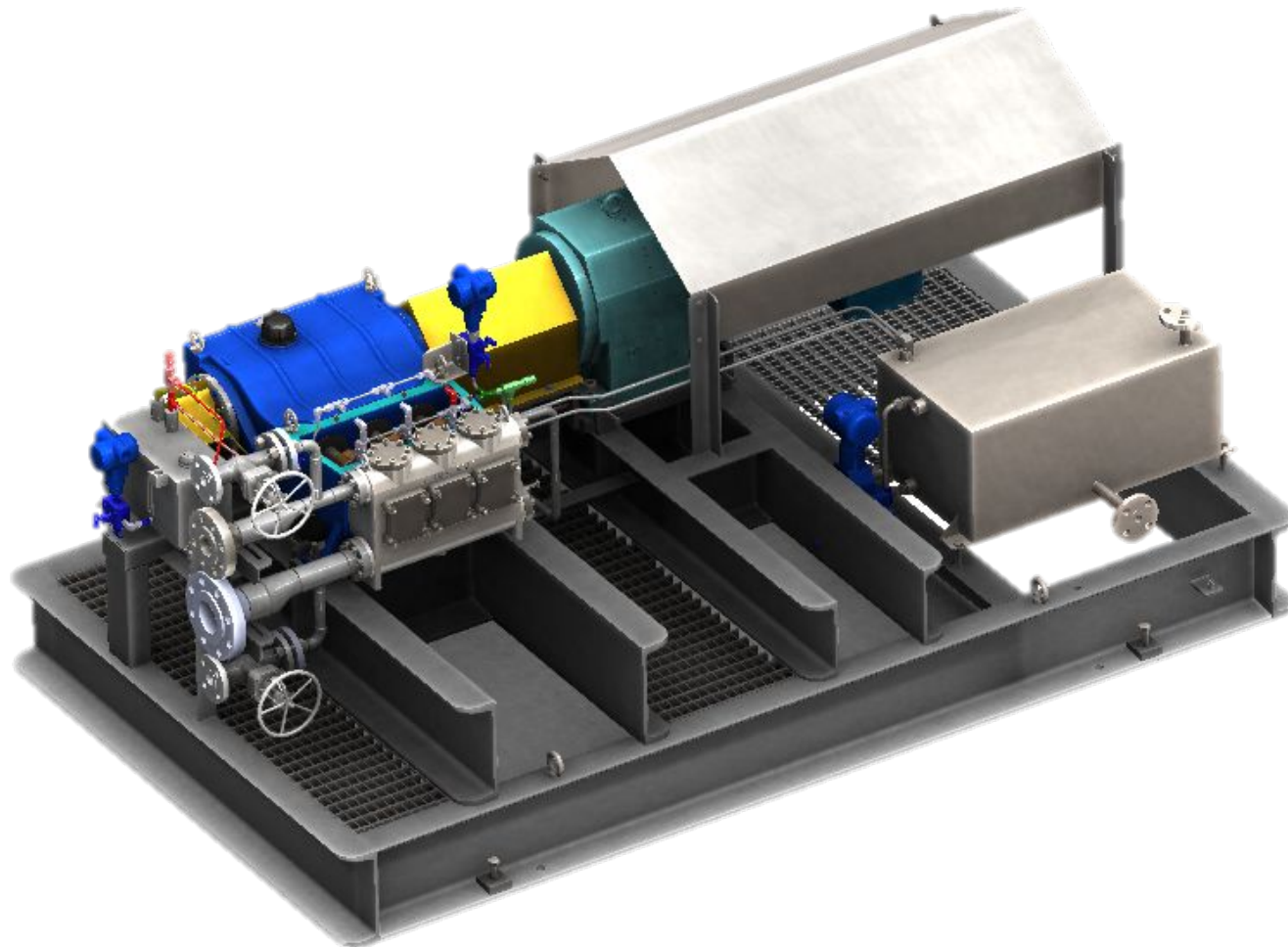
Booster Pump on Skid



Forced Lube



Package options



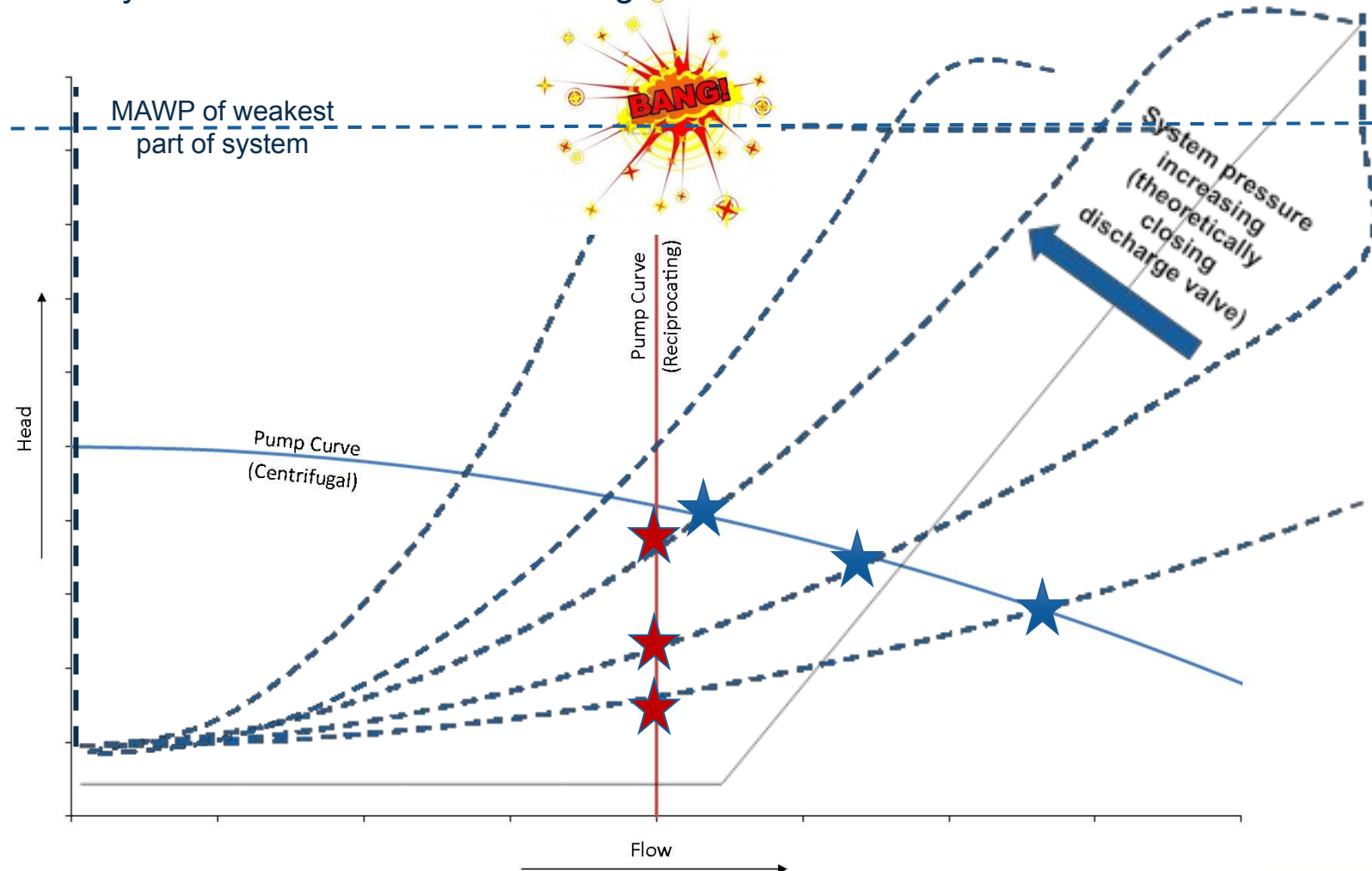
AUXILIARIES



Pressure Safety

REMEMBER THIS ... ?

- Theoretically unlimited head when discharge valve is closed



PSV

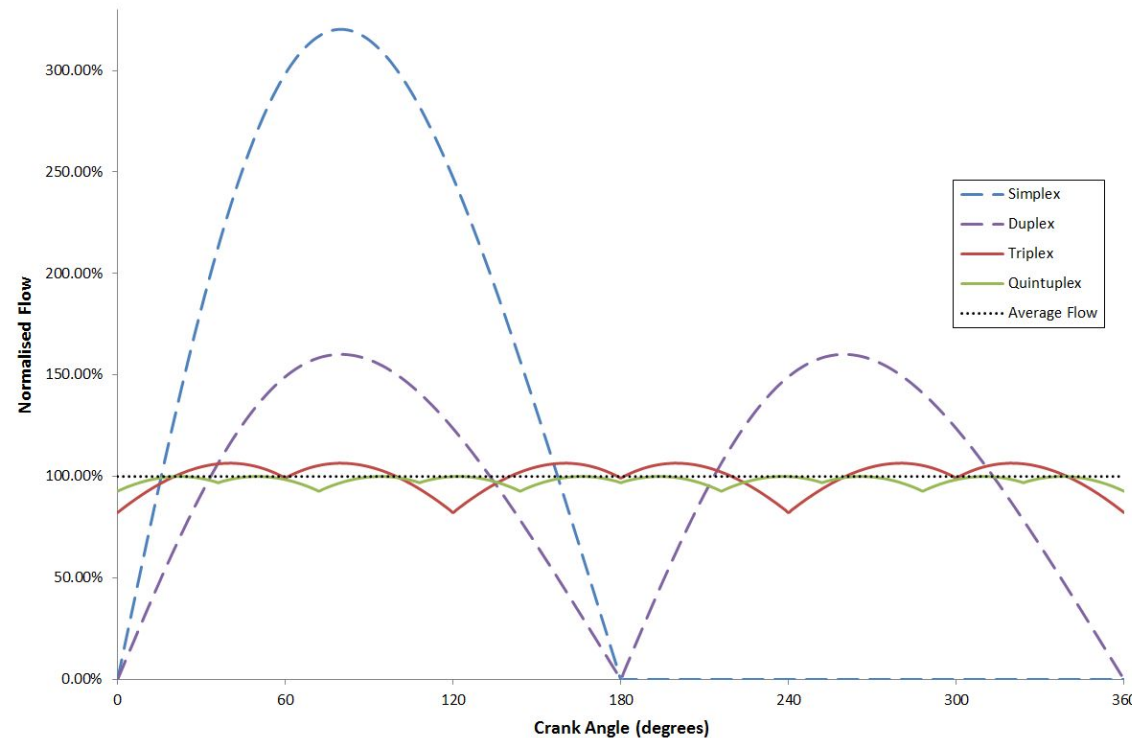


- Mandatory for reciprocating pumps: pressure spikes
- Fast response
- Must be closest thing to pump without any restrictions
- Can be mounted to pump head or in discharge line
- API 520/526 may be applicable
- Line between PSV and pump must not be prone to blockage
- Relief line should have little to no back pressure in the ideal case
- Relief to atmosphere or supply tank above liquid line
- Relief line should not go back to suction line
- 3 basic types: spring loaded, bellow and pilot – depending on back pressure



Pulsation Control

- Due to the nature of reciprocating pump action, flow pulses (unlike a centrifugal pump)
- The result is pulsations which are of different forms depending on number of plungers



Pulsation Dampening – Why?

- Process
 - Pressure pulsations in the process line may be undesirable for the application
- NPSH
 - In low NPSH applications a pressure drop during the suction cycle may cause cavitation
- Acceleration Head (Ha)
 - Reduces energy losses caused by Ha within the piping system.
- Structural
 - Mechanical stresses on pipework and infrastructure undesirable
- Booster Duty
 - Where the reciprocating pump is being boosted by a centrifugal pump, variations in suction flow/pressure are undesirable
- Noise Generation

- Second closest item to pump
- Recommended maximum distance from pump = 1m
- Can be mounted on pump head
- Vertical / horizontal orientation (depending on design)



Types Of Dampener

Bladder Type



Stores excess pressure/flow and expels when needed

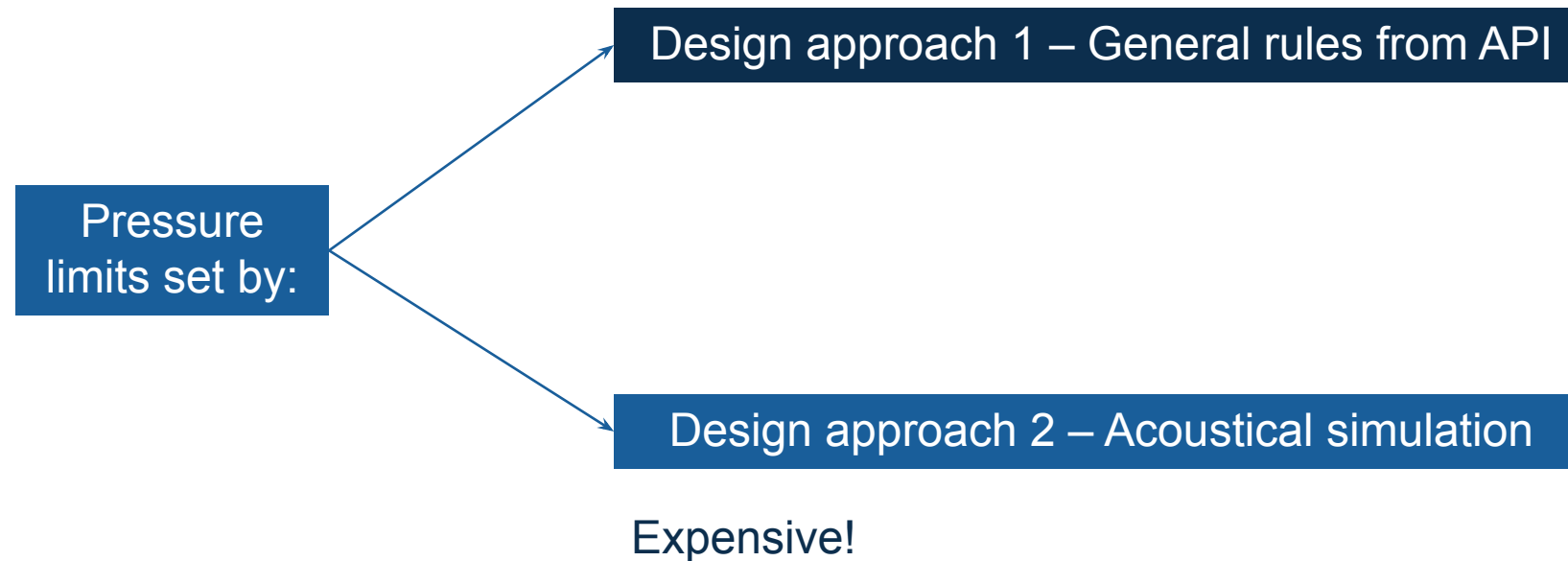
- Small: inexpensive
- Moveable parts: maintenance

Acoustic Type



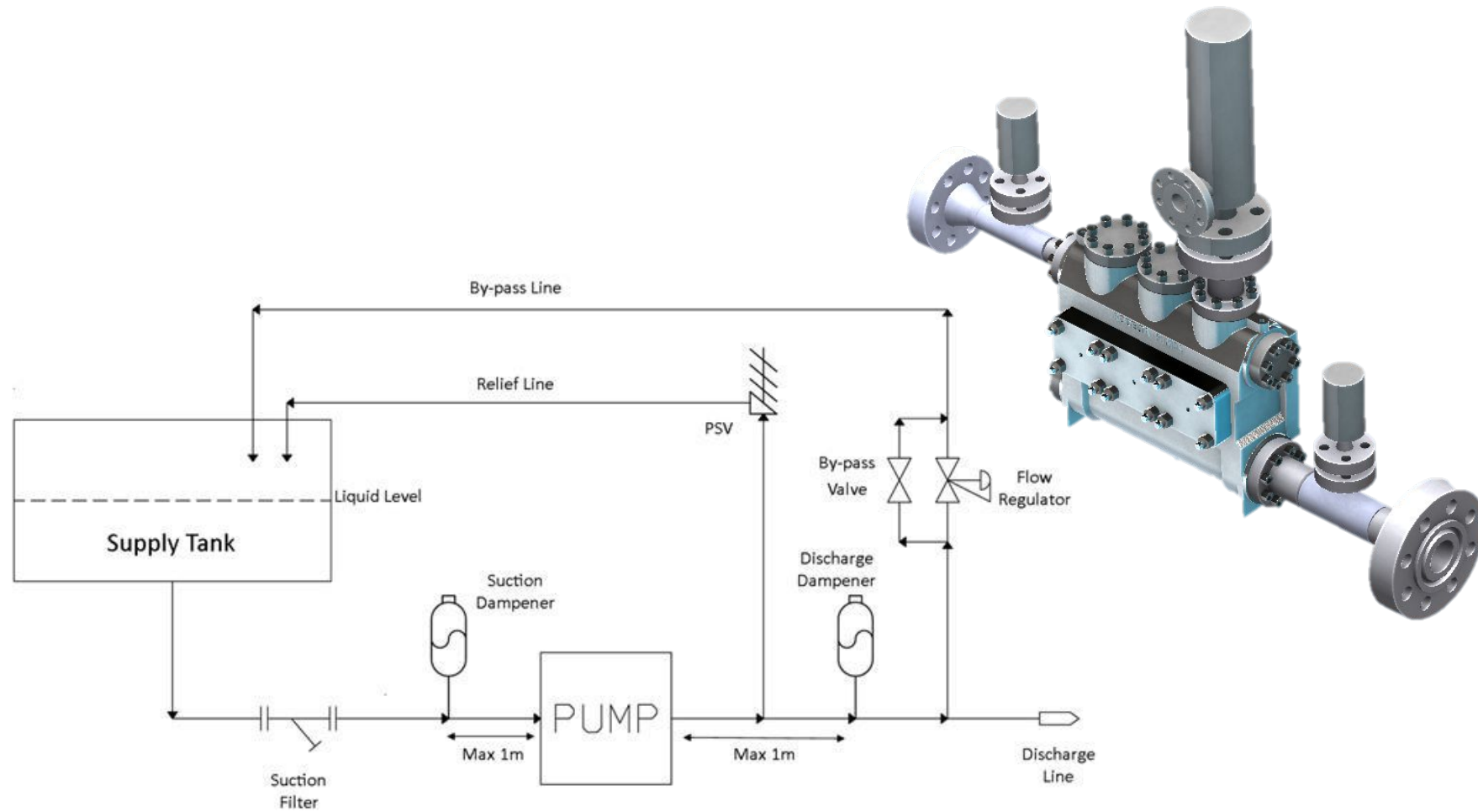
Impedes pressure waves from traversing through system

- Big: Expensive
- No moving parts: little maintenance



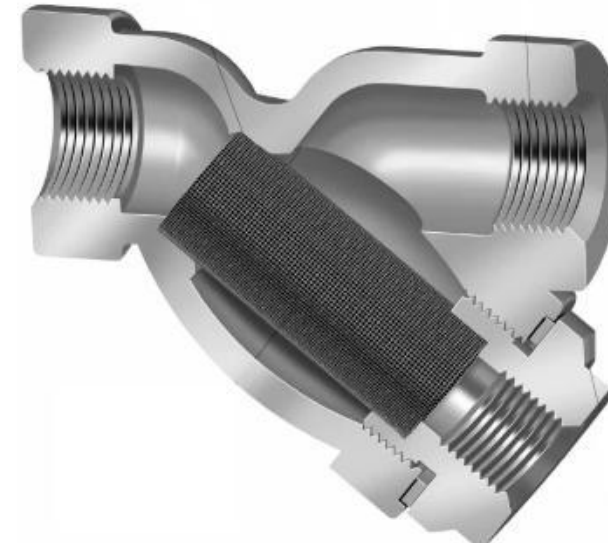
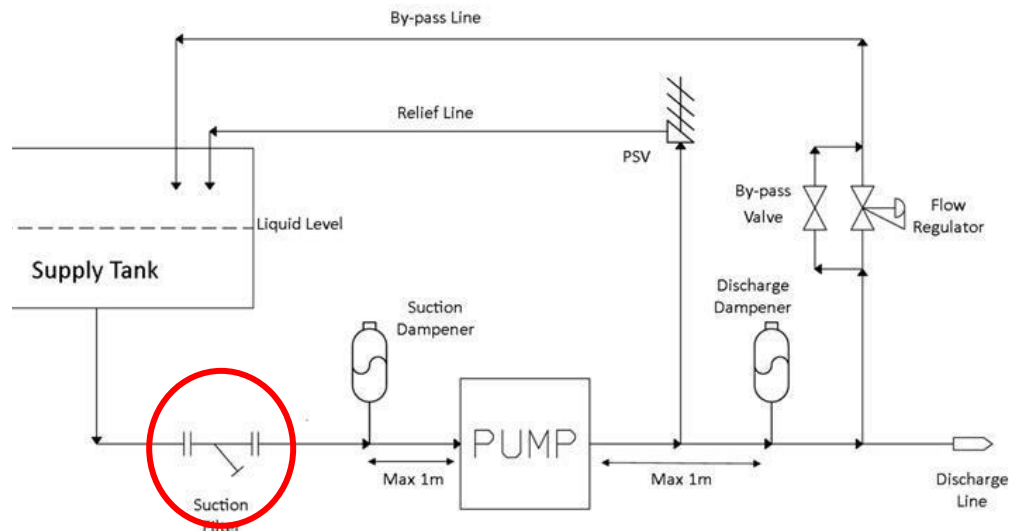
- The customer might actually specify a set of pulsation limits themselves

AUXILIARY LAYOUT



Suction Strainer / Filter

- Use not recommended
- Reduces NPSH and could block => cavitation/ dry running
- However, might be necessary to protect pump from excessive solid content
- Choose coarsest mesh viable
- Ideal to include differential pressure switch over strainer



Coming Attractions 😊

“Vertical Pumps (VS1, VS4, VS6)”

Thurs 24th Apr – 08.00 UK BST (UTC+1) (Eastern Hemisphere) & 17.00 UK BST (UTC+1)
(Western Hemisphere)

Aimed at Process and Mechanical Engineers, and Consultant Engineers who specify pumping equipment as well as Applications & Sales Engineers selecting and quoting them.

While engineers generally have a good understanding of horizontal pumps, their exposure to vertical pumps is more limited and as a result they are frequently misunderstood and under-utilised.

This course will look to put that right and explain the features and benefits of vertical pumps and how they can frequently be problem solvers.



Specialist for Pumping Technology

Q & A

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www.ruhrpumpen.com

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RUHRPUMPEN AT A GLANCE

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OFFICES IN
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**MANUFACTURING
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IN 10 COUNTRIES**

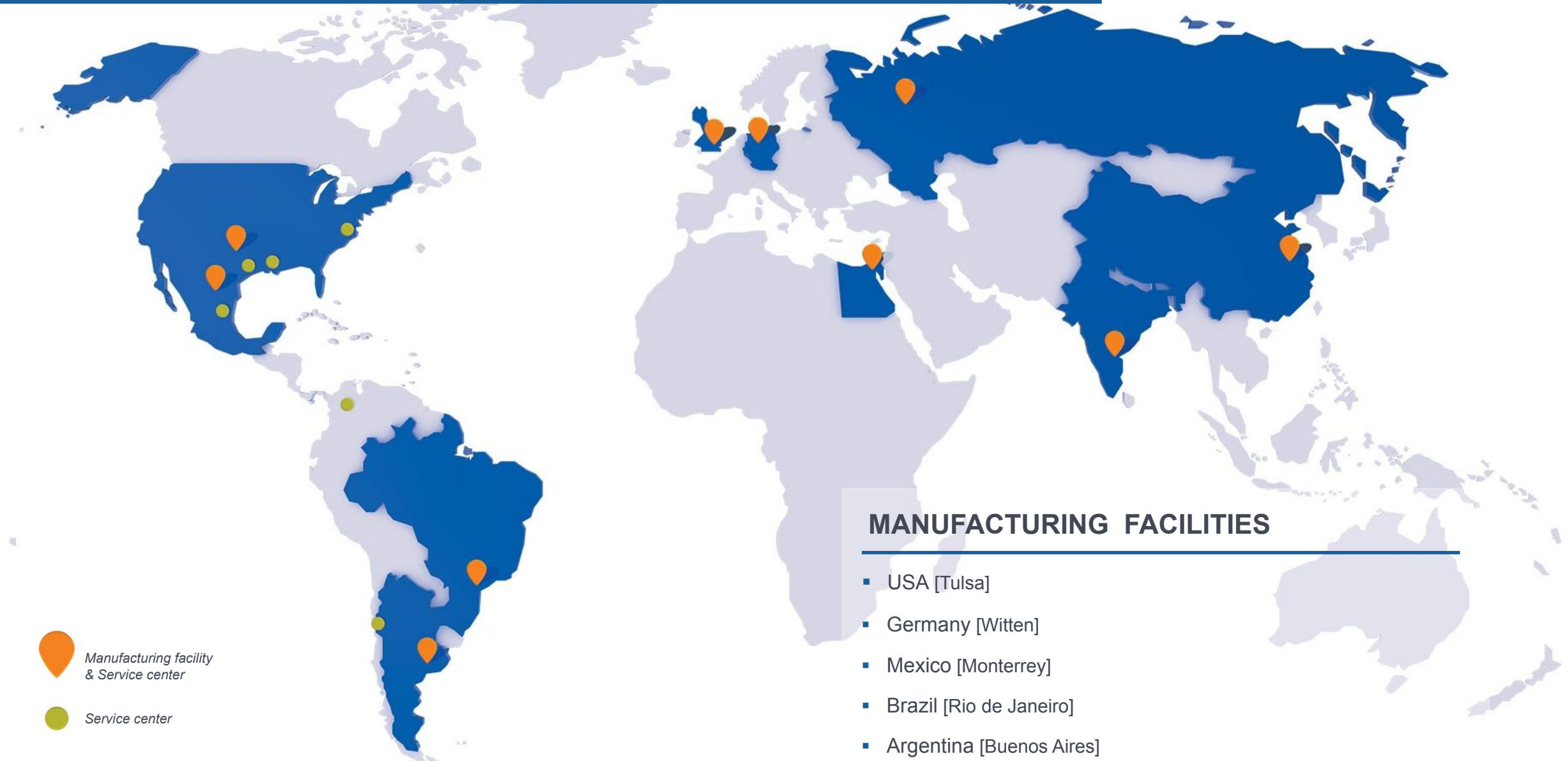
**+70 YEARS
OF EXPERIENCE**

**+2,000
EMPLOYEES**

**15 SERVICE
CENTERS**

+70,000 PUMPING SOLUTIONS INSTALLED WORLDWIDE

A GLOBAL COMPANY



MARKETS WE SERVE

Our commitment to create innovations that offer reliable solutions to our customers allow us to provide a complete range of pump systems to support **core markets** as:





OUR PUMP LINES

Ruhrpumpen offers a broad range of highly engineered and standard pumping products that meet and exceed the requirements of the most demanding quality specifications and industry standards.

Our pumps can handle head requirements as high as 13,000 ft (4,000 m) and capacities up to 300,000 gpm (68,000 m³/hr). Moreover, our pump designs cover temperatures from cryogenic temperatures of -310 °F (-196 °C) up to 752 °F (400 °C).

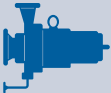


Products include:

- Single Stage Overhung Pumps
- Between Bearings Pumps
- Horizontal Multi-Stage Pumps
- Vertical Multi-Stage Pumps
- Vertical Mixed Flow & Axial Flow Pumps
- Positive Displacement Pumps
- Full Range of Industrial Pumps
- Submersible Pumps
- Magnetic Drive Pumps
- Decoking Systems
- Packaged Systems
- Fire Systems



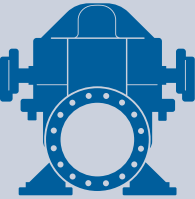
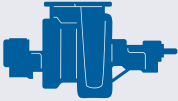
OVERHUNG PUMPS

CATEGORY	RP MODEL	DESIGN STANDARD	
Sealless Magnetic Drive Pumps	CRP-M / CRP-M-CC	ISO 2858 & 15783 HI design (OH11)	
	SCE-M	API 685	
Foot Mounted OH1 and General End Suction Pumps	IPP	HI design (OH1)	
	CPP / CPP-L	HI design (OH1) ANSI B73.1	
	CPO / CPO-L	HI design (OH1) ANSI B73.1	
	CRP	HI design (OH1) ISO 2858 & 5199	
	GSD	HI design (OH0)	
	SHD / ESK / SK / SKO SKV / ST / STV	HI design (OH1)	
	SWP	HI design (OH3A)	
Centerline Mounted	SCE	API 610 (OH2)	
Vertical In-Line Pumps	SPI	API 610 (OH3)	
	IVP / IVP-CC	HI design (OH4 / OH5)	
	IIL	HI design (OH5) Dimensionally compliant with ANSI B73.2	
	SPN	API 610 (OH5)	





BETWEEN BEARING PUMPS

CATEGORY		RP MODEL	DESIGN STANDARD	
1 and 2 stage	Axially split	HSC / HSD / HSL HSR / ZW	HI design (BB1)	
		HSM	HI design (BB3)	
		ZM / ZMS ZLM / ZME	API design (BB1)	
	Radially split	HVN / J	API design (BB2)	
		RON / RON-D	API design (BB2)	
Multi-stage	Axially split	SM / SM-I	API design (BB3)	
		JTN	API design (BB3)	
	Radially split <i>single casing</i>	GP	API design (BB4)	
	Radially split <i>double casing</i>	A LINE	API design (BB5)	





VERTICAL PUMPS

CATEGORY		RP MODEL	DESIGN STANDARD	
Single casing	Diffuser	VTP	HI & API 610 (VS1)	
		VCT	HI & API 610 (VS1)	
		HQ	HI & API 610 (VS1)	
		VLT	HI & API 610 (VS1)	
	Volute	DSV / DX	HI & API 610 (VS2)	
	Discharge through column – Axial flow	VAF	HI & API 610 (VS3)	
	Separate discharge line	VSP / VSP-Chem	HI & API 610 (VS4)	
Double casing	Diffuser	VLT / VMT	HI & API 610 (VS6)	
	Volute	DSV / DX	HI & API 610 (VS7)	
Submersible pumps		SMF	HI design (OH8A)	
		VLT-Sub / VTP-Sub	HI design (VS0)	





SPECIAL SERVICE PUMPS

CATEGORY	RP MODEL	DESIGN STANDARD	
Pitot tube pumps	COMBITUBE	HI design	
Reciprocating pumps	RDP	API 674 ISO 13710	
Vertical turbine generator	VTG	HI design (VS6)	
Barge	LS BARGE	HI design	
Floating dock pumps	ZVZ	HI design	
	LVZ	HI design	
Cryogenic pumps	SVNV	-	
	VTG Cryogenic	-	
	VLT Cryogenic VLTV	-	
Pre-packaged fire pump systems	Fire systems incorporate pumps, drivers, control systems and pipework in a single container. They can be skid mounted, with or without enclosure and supplied with electric motor or diesel engine.		NFPA-20-850 UL and FM approved components

